# Chapter -11

# WE LEARN ABOUT

- 11.1 Introduction
- 11.2 Zeroth law of
  Thermodynamics
  (Thermodynamic state,
  Variables, equations of
  state)
- 11.3 Thermodynamic Process(First law of thermodynamics,

Applications of first law, specific heat capacities)

- 11.4 Work done by the thermodynamical process
- 11.5 Cyclic and non cyclic process

(Heat engine, refrigerator, carnot cycle)

# THERMODYNAMICS

# **Briefintroduction**

sadi carnot was a French physicist, who gave the first successful theoretical account of heat engines, now known as the Carnot cycle, there by laying the foundations of the second law of thermodynamics. He is often described as the " Father of thermodynamics", being responsible for such concepts as Carnot efficiency, Carnot theorem, Carnot heat engine, and others. In 1824 the principle of conservation of energy was still immature and controversial, and an exact formulation of the first law of thermodynamics was still more than a decade away. The mechanical equivalent of heat was not identified for another two decades. The prevalent theory of heat was the caloric theory, which regarded heat as a sort of weightless, invisible fluid that flowed when out of equilibrium.



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## CLASS- XII THERMODYNAMICS

#### **11.1.1 INTRODUCTION**

In previous chapter we have studied thermal properties of matter. In this chapter we shall study laws that govern thermal energy. We shall study the processes where work is converted into heat and vice versa. In winter, when we rub our palms together, we feel warmer; here work done in rubbing produces the 'heat'. Conversely, in a steam engine, the 'heat' of the steam is used to do useful work in moving the pistons, which in turn rotate the wheels of the train.

In physics, we need to define the notions of heat, temperature, work, etc. more carefully. Historically, it took a long time to arrive at the proper concept of 'heat'. Before the modern picture, heat was regarded as a fine invisible fluid filling in the pores of a substance. On contact between a hot body and a cold body, the fluid (called caloric) flowed from the colder to the hotter body ! This is similar to what happens when a horizontal pipe connects two tanks containing water up to different heights. The flow continues until the levels of water in the two tanks are the same. Likewise, in the 'caloric' picture of heat, heat flows until the 'caloric levels' (i.e., the temperatures) equalise.

In time, the picture of heat as a fluid was discarded in favour of the modern concept of heat as a form of energy. An important experiment in this connection was due to Benjamin Thomson (also known as Count Rumford) in 1798. He observed that boring of a brass cannon generated a lot of heat, indeed enough to boil water. More significantly, the amount of heat produced depended on the work done (by the horses employed for turning the drill) but not on the sharpness of the drill. In the caloric picture, a sharper drill would scoop out more heat fluid from the pores; but this was not observed. A most natural explanation of the observations was that heat was a form of energy and the experiment demonstrated conversion of energy from one form to another–from work to heat.

deals with the concepts of heat and temperature and the inter-conversion of heat and other forms of energy. Thermodynamics is a macroscopic science. It deals with bulk systems and does not go into the molecular constitution of matter. In fact, its concepts and laws were formulated in the nineteenth century before the molecular picture of matter was firmly established. Thermodynamic description involves relatively few macroscopic variables of the system, which are suggested by common sense and can be usually measured directly. A microscopic description of a gas, for example, would involve specifying the co-ordinates and velocities of the huge number of molecules constituting the gas. The description in kinetic theory of gases is not so detailed but it does involve molecular distribution of velocities. Thermodynamic description of a gas, on the other hand, avoids the molecular description altogether. Instead, the state of a gas in thermodynamics is specified by macroscopic variables such as pressure, volume, temperature, mass and composition that are felt by our sense perceptions and are measurable<sup>™</sup>.

The distinction between mechanics and thermodynamics is worth bearing in mind. In mechanics, our interest is in the motion of particles or bodies under the action of forces and torques. Thermodynamics is not concerned with the motion of the system as a whole. It is concerned with the internal macroscopic state of the body. When a bullet is fired from a gun, what changes is the mechanical state of the bullet (its kinetic energy, in particular), not its temperature. When the bullet pierces a wood and stops, the kinetic energy of the bullet gets converted into heat, changing the temperature of the bullet and the surrounding layers of wood. Temperature is related to the energy of the internal (disordered) motion of the bullet, not to the motion of the bullet as a whole.

■ Thermodynamics may also involve other variables that are not so obvious to our senses e.g. entropy, enthalpy, etc., and they are all macroscopic variables.

Thermodynamics is the branch of physics that

## 11.1.1 HEAT AND TEMPERATURE

Heat is a form of energy called thermal energy.

When we bring a hot body in thermal contact with a cold body, then temperature of the hot body decreases and temperature of the cold body increases. The energy of the hot body decreases and that of the cold body increases. This transfer of energy takes place until the two bodies attain a common temperature, showing that the two bodies are at the same thermal condition.

So heat flows from a body at higher temperature to a body at lower temperature. This leads to the definition of heat.

**Definition of Heat:** The energy which is transferred between a system and its surroundings, as a I result of temperature difference only, is called heat.

Unit: joule in SI, Calorie in CGS system.

Dimensional formula: [ML<sup>2</sup>T<sup>-2</sup>].

Note:

Heat is certainly energy, but it is the energy in transit.

#### **Definition of Temperature:**

Temperature is defined as the thermal condition of a body which determines its ability to transfer heat to other bodies.

(a) Temperature is the measure of degree of hotness or coldness of a body.

(b) Temperature determines the direction of net flow of heat.

Unit: Kelvin (K) in absolute scale.

**Dimensional formula** [K] or  $[\theta]$ .

### 11.1.2 UNITS OF HEAT

Various units of heat are obtained by choosing different units of mass and temperature. The most commonly used unit is calorie.

**Calorie :** It is the unit of measuring heat. Calorie is generally defined as the amount of heat required by one gram of water to rise its temperature by

#### 1 °C.

In fact, one gram of water does not require die same amount of heat to rise the temperature by 1°C at all ranges of temperature. When one gram of water is heated from 0°C to 100°C, the mean value of the amount of heat required for 1°C rise of temperature is found to be the same as it requires between 14.5°C and 15.5°C. Hence mean calorie is defined as

**Def:** "The amount of heat required by one gram of water to rise, its temperature from 14.5°C to 15.5°C (or 58.1°F to 59.9°F) at a pressure of 1 atm."

#### **11.1.3 THERMODYNAMIC SYSTEMS**

To study the relation between the heat and mechanical work, a system is required. This relation can be studied by studying the changes in the properties of a system due to exchange of energy in the form of work.

A system is defined as a region in space. The region may contain a collection of large number of atoms or molecules with in a real or imaginary boundary.

**Ex:** A gas or vapour enclosed in a cylinder having a movable piston.

#### Surroundings:

The medium or matter or vacuum that surrounds the system which may participate in the process of exchange of matter or energy or both with the system.

#### **11.1.4 THERMAL EQUILIBRIUM**

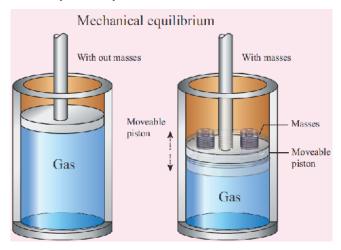
When a hot cup of coffee is kept in the room, heat flows from coffee to the surrounding air. After some time the coffee reaches the same temperature as the surrounding air and there will be no heat flow from coffee to air or air to coffee. It implies that the coffee and surrounding air are in thermal equilibrium with each other. Two systems are said to be in thermal equilibrium with each other if they are at the same temperature, which will not change with time.

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#### Mechanical equilibrium:

Consider a gas container with piston as shown in Fig. When some mass is placed on the piston, it will move downward due to downward gravitational force and after certain humps and jumps the piston will come to rest at a new position. When the downward gravitational force given by the piston is balanced by the upward force exerted by the gas, the system is said to be in mechanical equilibrium. A system is said to be in mechanical equilibrium if no unbalanced force acts on the thermodynamic system or on the surrounding by thermodynamic system.



# Mechanical equilibrium

#### **Chemical equilibrium:**

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If there is no net chemical reaction between two thermodynamic systems in contact with each other then it is said to be in chemical equilibrium.

# Thermodynamic equilibrium:

If two systems are set to be in thermodynamic equilibrium, then the systems are at thermal, mechanical and chemical equilibrium with each other. In a state of thermodynamic equilibrium the macroscopic variables such as pressure, volume and temperature will have fixed values and do not change with time.

#### 11.1.5 THERMODYNAMIC STATE VARIABLES

In mechanics velocity, momentum and acceleration are used to explain the state of any moving object. In thermodynamics, the state of a thermodynamic

system is represented by a set of variables called thermodynamic variables.

**Examples:** Pressure, temperature, volume and internal energy etc.

The values of these variables completely describe the equilibrium state of a thermodynamic system. Heat and work are not state variables rather they are process variables.

There are two types of thermodynamic variables: Extensive and Intensive

Extensive variable depends on the size or mass of the system.

**Example:** Volume, total mass, entropy, internal energy, heat capacity etc.

Intensive variables do not depend on the size or mass of the system.

**Example:** Temperature, pressure, specific heat capacity, density etc.

## **11.1.6 EQUATION OF STATE:**

The equation which connects the state variables in a specific manner is called equation of state. A thermodynamic equilibrium is completely specified by these state variables by the equation of state. If the system is not in thermodynamic equilibrium then these equations cannot specify the state of the system

An ideal gas obeys the equation PV = NkT at thermodynamic equilibrium. Since all four macroscopic variables (P,V,T and N) are connected by this equation, we cannot change one variable alone. For example, if we push the piston of a gas container, the volume of the gas will decrease but pressure will increase or if heat is supplied to the gas, its temperature will increase, pressure and volume of the gas may also increase.

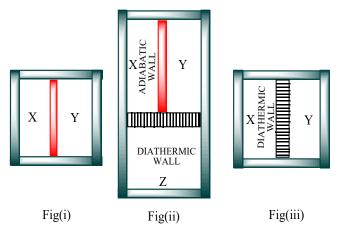
There is another example of equation of state called van der Waals equation. Real gases obey this equation at thermodynamic equilibrium. The air molecules in the room truly obey van der Waals equation of state. But at room temperature with low density we can approximate it into an ideal gas.

# **11.2.1 ZEROTH LAW OF THERMODYNAMICS**

**Def:** If two systems are in thermal equilibrium with a third system separately then they must be in thermal equilibrium with each other.

Consider two systems X and Y separated from each other by an adiabatic wall which does not allow the heat energy to pass through. The systems are not influenced by each other or influenced by the surroundings. So they are in separate state of equilibrium with different temperatures  $T_1$  and  $T_2$ , Fig (i). When this combination is arranged on another system Z with a diathermic wall which allows the heat energy to pass through as shown in the fig (ii). Now the two systems X and Y are in thermal contact with Z separately. Due to exchange of heat energy between systems X and Z they attain thermal equilibrium showing that these two are at same temperature T. Similarly system Y and system Z attain thermal equilibrium due to exchange of heat energy. The systems Y and Z attain the same temperature T.

The adiabatic wall between the systems X and Y is replaced by another diathermic wall and the combination is seperated from the system Z as shown in fig (iii). It is observed that no further changes in their temperatures showing that there is no exchange of heat energy between the systems X and Y. As they are at same temperature the two systems X and Y are said to be in thermal equilibrium.



Thus the temperature is defined as "the property which determines whether a system is in thermal equilibrium or not with the neighbouring system". If the two systems are at different temperature they are not in thermal equilibrium.

The property of thermal equilibrium is used in the measurement of temperature.

i) Zeroth law of thermodynamics, states that 'two systems in thermal equilibrium with a third system separately are in thermal equilibrium with each other'. R.H. Fowler formulated this law in 1931 long after the first and second I thermodynamics were stated and so numbered.

ii) The Zeroth Law clearly suggests that when two systems A and B are in thermal equilibrium, there must be a physical quantity that has the same value for both. The thermodynamic variable whose value is equal for two systems in thermal equilibrium is called temperature (T). Thus, if A and B are separately in equilibrium with C,  $T_A = T_C$  and  $T_B = T_C$ . This implies that  $T_A = T_B$  i.e. the systems A and B are also in thermal equilibrium.

# 11.2.2 JOULES LAW AND MECHANICAL]EQUIVA-LENT OF HEAT

### **Statement of Joule's Law :**

Whenever work is done against friction, heat is generated. The amount of heat generated (H) is directly proportional to the work done (W).

If w is the amount of mechanical work done and H is the amount of heat produced, then

### W $\alpha$ H or W = JH

Here J is constant of proportionality which is known as Joule's constant or Mechanical equivalent of heat If H= 1, than J = W

So, Joule's mechanical equivalent of heat is defined as the amount of work required to be done to produce a unit quantity of heat.

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#### Significance:

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Whenever heat is gained or lost by a system during some process, the gain or loss of heat can be taken to be equivalent to some amount of mechanical work done. In this way heat is included as a form of energy (thermal energy) in the solutions of the law of conservation of energy.

If H is measured in calories and W in joules, then J = 4.186 J cal<sup>-1</sup> If, W is measured in ergs then  $J = 4,186 \times 10^7 \text{ erg cal}^{-1}$ 

J is not a physical quantity. It is a conversion factor to convert units of work from one system to another.

The value of J=1 in SI where both W& H are measured in Joules.

In SI we write H = W since H and work are measured in Joules

#### Problem

A person of mass 60 kg wants to lose 5kg by going up and down a 10 m high stairs. Assume he burns twice as much fat while going up than coming down. If 1 kg of fat is burnt on expending 7000 kilo calories, how many times must he go up and down to reduce his weight by 5 kg?

Work done in moving up = mgh

Work done in moving down = mgh/2

Total work done,  $=\frac{\overline{3}}{2}$  mgh  $=\frac{3}{2}$  x 60 x 10 x 10 N number of trips

Sol:

5 x 7000 x 10<sup>3</sup> x 4.2 J = 60 x 15 x 10 x N N =  $\frac{21 \times 7 \times 10^6}{9000}$  x 10<sup>3</sup> = 16.3 x 10<sup>3</sup> times

#### **Problem:**

A lead bullet of mass 21 g travelling at a speed of 100 ms<sup>-1</sup> comes to rest in a wooden block. If no heat is taken away by the wood, find the rise in temperature of the wood.

(Specific heat of lead = 0.03 calorie/g °C.)

Sol:

kinetic energy of the bullet = heat gained by the bullet  $\frac{1}{2}$  mv<sup>2</sup> = ms $\Delta t$ 

$$\Delta t = \frac{v^2}{2s} = \frac{(100)^2}{2 \times 0.03 \times 4.2 \times 1000} = 39.68^{\circ}c.$$

#### 11.2.3 HEAT, INTERNAL, ENERGY AND WORK:

The three terms ; heat, internal energy and work will be used very commonly in this chapter. Therefore, it is important to understand them.

As we all know, heat is energy that flows from higher temperature to lower temperature. This flow is only because of difference in temperatures. We may thus define Heat as a form of energy in transit from hot to cold.

Every bulk system consists of a large number of molecules.

**Internal energy** of a system is the total energy possessed by the system due to molecular motion and molecular configuration.

It is represented by U.

The energy due to molecular motion is called internal kinetic energy  $U_k$ . The motion includes translational, rotational and vibrational motion of the molecules. The energy due to molecular configuration is called internal potential energy,  $U_p$ . Thus,

$$U = U_k + U_p$$

In case of an ideal gas or perfect gas, we assume that intermolecular forces are zero. Therefore, no work is done, whatsoever , in changing the distance between the molecules. Thus,  $U_p = 0$ . Hence, internal energy of an ideal gas consists only of internal kinetic energy-which depends only on temperature of the gas.

In a real gas, intermolecular forces are not negligible. Therefore, a definite amount of work has to be done in changing the distance between the molecules. Thus, internal energy of a real gas is sum of internal kinetic energy and internal potential energy of the molecules of the gas. It would obviously, depend on both, the temperature and volume of the gas. The following points regarding internal energy should be clearly understood :

(i) Internal energy of a system is a macroscopic state variable of the system. The internal energy of a given mass of gas depends on its state described by specified values of pressure, volume and temperature.

(ii) Internal energy of a system does depend on state of the system, but not on how that state was achieved or not on history of achieving the state, i.e., not on the path taken to arrive at that state.

(iii) In thermodynamics, the kinetic energy of the system as a whole is not relevant. It means if the container of the gas is moving as a whole with some velocity, the kinetic energy of the container is not to be included in internal energy.

(iv) The internal energy of a real gas can be changedby changing any of the macroscopic state variables ofthe gas.

Two ways of changing the state and hence internal energy of a gas are :

(a) Heating the cylinder containing the gas or keeping the cylinder in contact with a body at higher temperature. Some heat flows from hotter body to the gas on account of temperature difference. Therefore, internal energy of the gas increases.

(b) Pushing the piston of the cylinder containing gas in the upward direction. Some work is done by the gas, due to which the internal energy of the gas decreases.

Note that both these things could happen in the reverse direction too. For example, if the gas were in contact with a body at lower temperature, some heat would flow from gas to the surroundings resulting in fall in temperature and hence decrease in its internal energy. Similarly, if the piston were pushed downwards, work will be done on the gas. Therefore, internal energy of the gas would increase.

We observe that heat and work are two different modes of changing state of a thermodynamical system

and hence changing internal energy of the system.

Hence, we conclude that heat and work in thermodynamics are not state variables. They are two modes of energy transfer to or from a system resulting in change in internal energy of the system- which is tt state variable.

#### NOTE:

- Out of heat, internal energy and work, only internal energy of the system is a state variable. The other two, i.e., heat and work are two modes of energy transfer to or from a system. This energy transfer would result in the change of internal energy of the system.
- Internal energy of an ideal gas consists only of internal K.E. – which depends only on temperature of the gas.
- Internal energy of a real gas is sum of internal K.E. and internal P.E. of the molecules of the gas. It would therefore, depend on the temperature and volume of the gas.

# 11.2.4 THERMODYNAMIC STATE VARIABLES AND EQUATION OF STATE

**Themodynamic state variables** of a system are the parameters which describe equilibrium states of the system. For example, equilibrium state of a gas is completely specified by the values of pressure, volume, temperature, mass and composition (if there is a mixture of gases). The various state variables of a system are not necessarily independent.

The Equation of State represents the connection between the state variables of a system. For example, the equation of state of an ideal/perfect gas is represented as

# $PV = \mu RT$

where  $\mu$  is number of moles of the gas and R is gas constant for one mole of the gas.

For a fixed amount of gas (i.e., for given p), there are only two independent variables of ideal gases,

say (P and V) or (T and V). The real gases may have more complicated equations of state.

Further, the thermodynamic state variables are of two types :

(i) Extensive state variables and

(ii) Intensive state variables.

Extensive variables change with the size of the system, but intensive variables do not.

For example, imagine a gaseous system in thermal equilibrium divided into two equal parts. The state variables, volume V, mass M and internal energy U which get halved in each part are extensive variables. The other state variables like pressure P, temperature T and density  $\rho$  which remain unchanged for each part are intensive variables.

# 11.2.5 QUASI STATIC PROCESS

A process or a change in the state variables of a thermodynamical system, which is, infinitely slow is called quasi – static process (meaning–nearly static). The system undergoes changes in its variables like P, V, T so slowly that it continues to be in thermal and mechanical equilibrium with its surroundings throughout all regions of the system and at all times.

Quasi – static process is only an idealised process, in which we imagine that at every stage, the system is an equilibrium state. This visualization is necessary because it is difficult to deal with non equilibrium states of the system.

In a quasi – static process, the difference in the pressure of the system and the external pressure is Infinitesimally small. Similarly, the difference between the temperature of the system and temperature of the surroundings is infinitesimally small. Therefore, a quadristatic process must he infinitely slow.

For example, to take a gas from the state (P, T) to another state (P', T'), via a quasi-static process, we change the external pressure/temperature by a very small amount and allow the system to equalise its pressure/temperature with the surroundings. Continue the process infinitely slowly till the final state (P'/ T') is attained.

Obviously, a quasi – static process is a hypothetical construct. The process must be infinitely slow, should not involve large temp, differences or accelerated motion of the piston of the container.

In our discussion further, we shall assume all thermodynamic processes to be quasi – static, unless stated otherwise.

#### **11.3.1 THERMODYNAMIC PROCESSES**

A thermodynamical process is said to take place when some changes occur in the state of a thermodynamic system, i.e,, the thermodynamic parameters of the system change with time.

A system can interact with its surroundings in several ways. The heat energy and work that come into play always obey the first law of thermodynamics.

Following are some of the important thermodynamic processes :

- 1. Isothermal Process is that which occurs at a constant temperature.
- 2. Adiabatic Process is that in which no heat enters or leaves the thermodynamic system during the change.
- 3. Isobaric Process is that which occurs at constant pressure.
- 4. Isochoric or Isovolumic Process is that which occurs at constant volume.

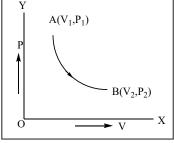
Summarises the four special thermodynamic processes.

S. No	Type of process	Feature
1.	Isothermal	Temperature constant
2.	Adiabatic	No heat flow between the system and the surroundings, i.e., $\Delta Q = 0$
3.	Isobaric	Pressure constant
4.	Isochoric	Volume constant

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# 11.3.2 INDICATOR DIAGRAM OR P - V DIAGRAM

The indicator diagram or P-V diagram represents the variation of volume V of a system with the pressure P of the system. Usually, we plot volume V along OX and pressure P along OY, as shown in Fig. The shape of PV diagram shall depend upon the nature of thermodynamical process, the system undergoes. In Fig, point A  $(V_1, P_1)$  represents initial state and the point B  $(V_2, P_2)$  represents final state of the system. The various points on the curve AB represent the intermediate states of the system in going from A to B.



### 11.3.3 FIRST LAW OF THERMODYNAMICS

Statement: "If the quantity of heat supplied to a system

is capable of doing work, then the quantity of heat absorbed by the system is equal the sum of the increase in the internal energy of the system, and the external work done by it".

Consider some amount of gas enclosed in a cylinder having thermally insulated walls fixed with a frictionless movable piston made of thermally insulated material. But it has a conducting bottom.

Let 'A' be the initial position of the piston and <sub>1</sub> be the initial internal energy of the gas. Let an amount of heat 'dQ' be added to the gas through the conducting bottom

The total initial thermal energy of the gas  $= U_1 + dQ$ 

The gas absorbs heat energy and expands the pushing the piston to a new position 'B'. The work done

by the gas in displacing the piston through a small distance dx is dW.

The internal energy of the system increases to  $U_2$  by absorbing the heat 'dQ'. Some of the internal energy is utilised in performing external work done (dW) in pushing the piston away. The internal energy changes to  $U_3$ .

The total energy after pushing =  $(U_3 + energy$  converted into work) j

According to law of conservation of energy

$$U_1 + dQ = U_2 = U_3 + dW$$

$$dQ = (U_3 - U_1) + dW$$

 $(U_3 - U_1)$  is the change in internal energy dU.

If an infinitesimally small amount of heat 'dQ' is added to the system (gas), corresponding change in internal energy is 'dU' and the work done by the gas is 'dW'.

Then 
$$dQ = dU + dW$$
.

This is the mathematical statement of first law of thermodynamics.

#### Sign convention

If the heat energy dQ is added to the system (gas) it is taken as positive (+dQ).

If the heat is given out (released) by the system it is taken as negative (-dQ).

If the work is done by the system (gas) it is taken as positive (+ dW).

If the work is done on the system (gas) by surroundings it is taken as negative (-dW).

The increase in internal energy is taken as positive (+dU).

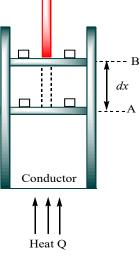
The decrease in internal energy is taken as negative (-dU).

#### Significance and limitations

1) This law introduces the concept of internal energy.

2) This law is applicable to all the three phases of matter (i.e., solid, liquid and gas).

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3) This law is applicable to any process in nature.

4) This law does not give any information about the direction of heat flow, between the hot and cold body, when they are in thermal contact.

5) This law tells that it is impossible to get work from any machine without giving it an equivalent amount of heat energy.

#### NOTE:

- Heat and work are two distinct modes of energy transfer to a system that results in change in its internal energy, (a) Heat is energy transfer due to temperature difference between the system and the surroundings, (b) Work is energy transfer brought about by means (e.g. moving the piston by raising or lowering some weight connected to it) that do not involve such a temperature difference.
- The internal energy U of a system can change through two modes of energy transfer : heat and work.
- First Law of Thermodynamics is simply the general law of conservation of energy applied to any system in which the energy transfer from or to the surrounding is taken into account.
- U is a state variable, ΔU depends only on the initial and final states and not on the path taken by the gas to go from one to the other. However, ΔQ and ΔW will, in general, depend on the path taken to go from the initial to final states. Form the First Law of Thermodynamics, it is clear that the combination, is however ΔQ ΔW, path independent.

# 11.3.4 Applications of the first law of thermodynamics

#### (a) Isothermal Process:

In an isothermal process, temperature remains constant. If the system is an ideal gas, whose internal energy U depends only on temperature, the internal energy shall remain constant, i.e., dU = 0. The first law of thermodynamics implies .....

$$dQ = dU + dW = 0 + dW = dW,$$

i.e. dQ = dW

i.e., heat supplied in an isothermal process is used entirely to do work against the external surroundings.

# (b) Adiabatic Process:

In an adiabatic process, no heat energy enters or leaves the system as it is well insulated, i.e., dQ = 0. The first law of therodynamics implies

dQ = dU + dW = 0 or dU = -dW

When a gas expands adiabatically, dW is positive. Therefore, dU must be negative, i.e., internal energy of the system would decrease and the gas will be cooled. The reverse is also true.

## (c) Isochoric Process:

In an isochoric process, volume of a system (such as a gas) is kept constant, dW = P(dV) = 0. The first law of thermodynamics implies

$$dQ = dU + dW$$
$$dQ = dU$$

If heat is absorbed by a system at constant volume, its internal energy increases by the same amount and vice-versa.

#### (d) Isobaric Process:

In an isobaric process, pressure is kept constant. For example, when a liquid boils, its pressure and temperature remain constant till whole of the liquid is converted into vapours.

 $V_i = initial volume of liquid$ 

 $V_{f}$  = final volume of vapours

P = constant pressure at which liquid converts $into vapours, then work done, <math>dW = P.dV = P (V_f - V_j)$ 

If m is mass of liquid and L is latent heat of vaporisation of liquid, then heat supplied for converting entire liquid into vapours, dQ = mL

From first law of thermodynamics

dQ = dU + dW

 $dU = dQ - dW = mL - P(V_f - V_i)$ 

This is the change in internal energy of the liquid on vaporisation.

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or

If

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#### (e) Cyclic Process:

In such processes, the system returns to its initial state after any number of changes.

In that case, no intrinsic property of the system would change. As internal energy of a system is a state variable and final state of the system is same as the initial state, therefore there is no change in internal energy of the system, i.e., dU = 0.

The first law of thermodynamics implies dQ = dU + dWdQ = dW (:: dU = 0)

... Net work done during a cyclic process exactly equals the amount of heat energy transferred.

In a cyclic process, the system returns to its initial state after any number of changes. Therefore, P-V diagram of a cyclic process will be a closed loop of any arbitrary shape.

#### (f) Melting Process:

When a solid melts into a liquid, its internal energy increases, which can be calculated from first law of thermodynamics.

Let m = mass of a solid, L = latent heat of the solid.

Amount of heat absorbed during the melting process, dQ = mL

When a substance melts, the change in its volume (dV) is very small and therefore, it can be neglected.

 $\therefore \qquad dW = P(dV) = Px \ 0 = 0$ 

According to first law of thermodynamics, dQ = dU + dW

 $\therefore$  mL = dU + 0 or dU = mL

Hence, the internal energy during the melting process increases by (mL).

Note that increase in internal energy during melting process is at constant temperature. Therefore, it must be due to increase in internal potential energy  $(U_p)$ . The internal kinetic energy  $(U_k)$  remains constant. (g) Boiling process

Using first law of thermodynamics, we can calculate increase in internal energy of a liquid in the

process of boiling. In boiling, a liquid changes into vapours at constant temperature and pressure. Suppose m = mass of a liquid at its boiling point,  $V_1 = volume$  of the liquid,

P = constant pressure at which boiling process occurs,

 $V_2$  = Volume of the same liquid in the vapour form under the same pressure,

L = Latent heat of vaporisation of the liquid.

: Work done in expansion,  $dW = P(dV) = P(V_2 - V_1)$ 

Heat absorbed by the liquid in the boiling process, dQ = mL

According to first law of thermodynamics,

$$dQ = dU + dW$$
$$dU = dQ - dW$$
$$dU = mL - P (V_2 - V_1)$$

Knowing m, L, P,  $V_1$  and  $V_2$ , we can calculate dU, i.e., increase in internal energy of the liquid in the boiling process. This is again due to increase in internal potential energy.

#### (h) Free Expansions

The free expansions consist of adiabatic processes in which no transfer of heat occurs between the system and its surroundings and no work is done on or by the system, i.e., dQ = 0 and dW = 0

According to first law of thermodynamics, change in internal energy of the system

$$dU = dQ - dW = 0$$

Note that free expansions cannot be eluted slowly and in a controlled way. Therefore, we cannot plot P - V diagram for such processes.

# 11.3.5 Specific heat of a gas at constant pressure : $C_n$

At constant pressure, the quantity of heat necessary to increase the temperature of unit mass of a gas through one degree is called specific heat of the gas at constant pressure.

If ' $\Delta Q$ ' is the quantity of heat required to rise the temperature of "m" mass of gas through ' $\Delta t$ ' at constant pressure.

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$$C_{p} = \frac{\Delta Q}{m \Delta t} \quad \begin{array}{c} CGS \text{ unit : } Cal / g \ ^{\circ}C}{SI \text{ unit: } J \text{ kg}^{-1}K^{-1}} \end{array}$$

Molar specific heat of a gas at constant pressure: C<sub>p</sub>

At constant pressure, the quantity of heat necessary to increase the temperature of one mole of a gas through one degree is catted molar specific heat or molar heat capacity of the gas at constant pressure,  $C_p$ )

Let ' $\Delta Q$ ' is the quantity of heat required to rise the temperature of 'n' moles of gas through ' $\Delta t$ ' at constant pressure. Then

$$C_{p} = \frac{\bigtriangleup Q}{n \bigtriangleup t}$$

If 'm' is the mass of gas considered and 'M' is its molecular weight then n = m/M.

$$C_{p} = \frac{M \bigtriangleup Q}{m \bigtriangleup t} = M c_{p}$$
  
C.G.S unit : Cal / mole °C  
SI unit: J mole<sup>-1</sup> K<sup>-1</sup>

# 11.3.6 Specific heat of a gas at constant volume : $C_v$

At Constant volume, the quantity of heat necessary to increase the temperature of unit mass of a gas through one degree is called the specific heat of the gas at constant volume. It is denoted by  $c_v$ . If ' $\Delta Q$ ' is the quantity of heat required to rise the temperature of 'm' mass of gas at constant volume through ' $\Delta t$ ' then

$$c_v = \frac{\Delta Q}{m \Delta t}$$
  
C.G.S unit : Cal / g°C  
SI unit: J kg<sup>-1</sup> K<sup>-1</sup>

# Molar specific heat of a gas at constant volume: C<sub>v</sub>.

At constant volume, the quantity of heat necessary to increase the temperature of one mole of a gas through one degree is called "Molar specific heat" or molar heat capacity of the gas at constant volume  $C_v$ 

If ' $\Delta Q$ ' is the quantity of heat required to rise the temperature of 'n' moles of a gas through 'At' at constant volume.

$$C_{\rm v} = \frac{\Delta Q}{n \Delta T}$$

If 'm' is the mass of the gas and 'M' is its molecular weight then

$$n = \frac{m}{M} \text{ then } C_v = \frac{M \bigtriangleup Q}{m \bigtriangleup T} = M c_v$$
  
C.G.S unit : Cal / mole °C  
SI unit: J mole<sup>-1</sup> K<sup>-1</sup>

### **11.3.7 LIMITS OF SPECIFIC HEAT OF A GAS**

Consider mass 'm' of a gas. Let  $\Delta Q$  units of heat raise the temperature of the gas through  $\Delta T$ . Then the specific heat of the gas is given by

$$\mathbf{c} = \frac{\Delta \mathbf{Q}}{\mathbf{n} \Delta \mathbf{T}} \qquad [\because \Delta \mathbf{Q} = \mathbf{mc} \ \Delta \mathbf{T}]$$

Consider a gas enclosed in a cylinder fitted with an air-tight and frictionless piston.

i) Let the gas be suddenly compressed. In this case, no heat is supplied to the gas. But there is an increase in the temperature of the gas.

$$\mathbf{c} = \frac{\Delta \mathbf{Q}}{\mathbf{n} \Delta \mathbf{T}} \qquad [\because \Delta \mathbf{Q} = \mathbf{0}]$$

ii) Let the gas be heated and allowed to expand. Suppose the 'fall in temperature due to expansion' is equal to the 'rise in temperature due to supplied'.

$$\therefore \qquad \mathbf{c} = \frac{\Delta \mathbf{Q}}{\mathbf{m} \times \mathbf{0}} = \infty \qquad [\because \Delta \mathbf{T} = \mathbf{0}]$$

iii) Let the gas be heated and allowed to expand suppose,in this case, the 'fall in temperature due to expansion' isless than the 'rise in temperature due to heat supplied'.The net effect will be a rise in temperature of the gas.

So, 
$$\Delta T$$
 is positive. Thus  $c = \left(\frac{\Delta Q}{m \Delta T}\right)$  is positive.

iv) Let the gas be heated and allowed to expand such that the 'fall in temperature due to expansion is more than the 'rise in temperature due to heat supplied'. The net effect will be a decrease in the temperature of the gas.

So  $\Delta T$  is negative. Thus,  $c = \left(\frac{\Delta Q}{m \Delta T}\right)$  is negative.

# 11.3.8. $C_p$ is Greater Than $C_v$

When a gas is heated at constant volume, no heat is spent in the expansion of the gas. The whole amount of heat is used to increase the temperature of the gas; increasing the internal energy.

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If  $(dQ)_v$  is heat supplied to n moles of a gas at Mont volume.

 $dU_1$  is the increase in internal energy

 $dT_1$  is the rise in temperature

n is the number of moles

C<sub>v</sub> is the molar specific heat at constant volume

Then  $(dQ)_v - dU_1 + 0 = n C_v dT_1$  ....(1)

When a gas is heated at constant pressure, the temperature of the gas increases and the volume also increases due to expansion.

Therefore a part of the heat supplied, to the gas is utilised to increase the temperature, increasing the internal energy and the other part is utilised in performing work against the external pressure during its expansion (dW)

If  $(dQ)_p$  is the heat supplied to the gas at constant pressure

dU<sub>2</sub> is increase in internal energy

 $dT_2$  is the rise in temperature

dW is the work done during the expansion

n is the number of moles

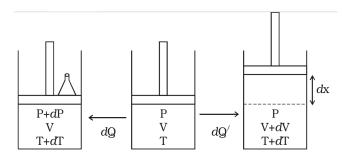
 $C_p$  is the molar specific heat at constant pressure  $(dQ)_p = n C_p dT_2 = dU_2 + dW$  ...(2) If the rise in temperature is same  $dT_1 = dT_2 = dT$ so internal energies  $dU_1 = dU_2$ 

From equations 1 and 2

# Relation between $C_p$ and $C_v$ (Meyer's relation)

Let us consider one mole of an ideal gas enclosed in a cylinder provided with a frictionless piston of area A. Let P, V and T be the pressure, volume and absolute temperature of gas respectively (Fig.).

A quantity of heat dQ is supplied to the gas. To keep the volume of the gas constant, a small weight is placed over the piston. The pressure and the temperature of the gas increase to P + dP and T + dT respectively. This heat energy dQ is used to increase the internal energy dU of the gas. But the gas does not do any work (dW = 0).



# Meyer's relation $dQ = dU = 1 \times C_v \times dT \qquad ... (1)$

The additional weight is now removed from the piston. The piston now moves upwards through a distance dx, such that the pressure of the enclosed gas is equal to the atmospheric pressure P. The temperature of the gas decreases due to the expansion of the gas.

Now a quantity of heat dQ' is supplied to the gas till its temperature becomes T + dT. This heat energy is not only used to increase the internal energy dU of the gas but also to do external work dW in moving the piston upwards.

$$\therefore$$
 dQ' = dU + dW

Since the expansion takes place at constant pressure,

$$dQ' = C_{p}dT$$
$$C_{p}dT = C_{v}dT + dW \qquad ... (2)$$

Work done, dW =force  $\times$  distance

$$= \mathbf{P} \times \mathbf{A} \times \mathbf{d}\mathbf{x}$$

dW = P dV (since  $A \times dx = dV$ , change in volume)

$$C_{u}dT = C_{u}dT + P dV \qquad \dots (3)$$

The equation of state of an ideal gas is

$$PV = RT$$

Differentiating both the sides

$$PdV = RdT$$
 ... (4)

Substituting equation (4) in (3),

$$C_{p}dT = C_{v}dT + RdT$$
$$C_{p} = C_{v} + R$$
$$C_{p} - C_{v} = R$$

This equation is known as Meyer's relation

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&

...(4)

# 11.4.1 Specific heat of gases in terms of

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Temperature is the measure of average kinetic energy of the molecules of a gas. The kinetic energy of a molecule is the sum of translational kinetic energy, vibrational kinetic energy and rotational kinetic energy. According to the law of equipartition of energy, the total energy is divided equally among the degrees of freedom of a molecule.

The average kinetic energy per molecule per degree =  $\frac{1}{2}$  KT.

where K is the Boltzmann's constant T is the average temperature.

Consider one mole of gas containing  $\rm N_{A}$  number (Avogadro number) of molecules.

The average kinetic energy per one mole per degree of freedom =  $\frac{1}{2}$  RT.

# (i) For a mono – atomic gas the degree freedom is 3.

 $\therefore$  The internal energy U =  $\frac{3}{2}$  RT

... The change in internal energy

$$\therefore \qquad \mathrm{dU} = \frac{3}{2} \,\mathrm{RdT} \qquad \dots(1)$$

Let a small quantity of heat dQ is transferred to the gas at constant volume so that only the internal energy is increased by dU. Hence dQ = dU.

Let the corresponding rise in temperature be dT.

... Molar specific heat at constant volume

$$C_{v} = \frac{dQ}{1 \times dT} = \frac{dU}{dT}$$

from equation(1)

$$\therefore \qquad C_v = \frac{dU}{dT} = \frac{3}{2} \frac{RdT}{dT} = \frac{3}{2} R \qquad ...(2)$$

But

 $\therefore C_{p} - C_{v} = R$ 

$$\therefore$$
  $C_{p} = R + C_{v}$ 

:. 
$$C_{p} = R + \frac{3}{2}R = \frac{5}{2}R$$
 ...(3)

For a monoatomic gas =

$$\gamma = \frac{C_{\rm P}}{C_{\rm V}} = \frac{\frac{5}{2}R}{\frac{3}{2}R} = \frac{5}{3} = 1.67$$

# (ii) For a diatomic gas the degrees of freedom is 5

Hence the internal energy for n mole of gas

$$U = \frac{5}{2} nRT$$
  
The change in internal energy  
$$dU = \frac{5}{2} RdT$$

$$C_v = \frac{dU}{ndT} = \frac{\frac{5}{2}nRdT}{ndT} = \frac{5}{2}R$$

But  $C_p = C_V + R$ 

$$C_{p} = \frac{5}{2}R + R = \frac{7R}{2}$$
 ...(6)

For a diatomic gas =  

$$\gamma = \frac{C_P}{C_V} = \frac{\frac{7}{2}R}{\frac{5}{2}R} = \frac{7}{5} = 1.4$$

(iii) For a triatomic gas the degree of freedom may be 6 or 7.

... The internal energy

$$U = \frac{6nRT}{2} = 3nRT \Rightarrow dU = 3nRdT$$

$$CV = \frac{dU}{nRT} = \frac{3nRdT}{ndT} = 3R$$

$$C_{-} = 3R + R = 4R$$

For a triatomic or polyatomic gas

$$\gamma = \frac{C_P}{C_V} = \frac{4R}{3R} = \frac{4}{3} = 1.33$$

# Expression of $C_{\rm p}$ and $C_{\rm v}$ in terms of adiabatic constant $\gamma$

Consider the relation  $C_p - C_v = R \rightarrow (1)$   $\frac{C_p}{C_v} = \gamma$   $\therefore$   $C_p = \gamma C_v \rightarrow (2)$ From (1) & (2)  $\gamma C_v - C_v = R$   $\therefore$   $C_v = \frac{R}{\gamma - 1} \rightarrow (3)$ from (2) and (3)  $C_p = \frac{\gamma R}{\gamma - 1}$ 

### **ISOTHERMAL OPERATION/CHANGE**

A change in pressure and volume of a gas without any change in its temperature, is called an isothermal change. In such a change, there is a free exchange of heat between the gas and its surroundings. When a gas in an enclosure is compressed, work is done on the gas. Some heat is produced and its temperature tends to rise. If temperature of the gas is to remain constant, heat produced must be lost to the surroundings. Similarly, when the pressure on the gas is decreased, it expands, work is done by the gas, some heat energy is spent. Therefore, the temperature of the gas tends to fall. To keep the temperature of the gas constant, it must gain heat from its surroundings. Obviously, for an isothermal change, there should be a free exchange of heat between the gas and its surroundings.

Hence, the two essential conditions for a perfect isothermal change are :

(i) the walls of the container must be perfectly conducting, to allow free exchange of heat between the gas and its surroundings,

(ii) the process of compression or expansion should be slow so as to provide time for the exchange of heat between the gas and its surroundings.

As both these conditions are difficult to be realised strictly in practice, therefore perfect isothermal changes are practically impossible

### Some Examples of isothermal changes

- Melting process is an isothermal change, because temperature of a substance remains constant during melting.
- 2. Similarly, boiling process is also an isothermal operation.
- 3. When a gas in a cylinder with perfectly conducting walls and perfectly conducting frictionless piston is compressed or allowed to expand so slowly that heat produced in compression or heat spent in expansion is exchanged with the surroundings, the changes are isothermal changes.

As in all isothermal operations, temperature is kept, constant, pressure (P) and volume (V) are related to each other by Boyle's Law; i.e.,

$$PV = constant*$$

or

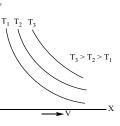
$$P_2V_2 = P_1V_1$$
 ...(1)

This is known as the equation of an isothermal

change.

If we plot a graph between V Y and P keeping temperature constant, we get a curve called an isothermal<sup>P</sup> curve or an isotherm for the given mass of gas at a given temperature.

In Fig., isotherms for three



different temperatures  $T_1$ ,  $T_2$ , and  $T_3$  are shown. From Fig, we find that the isotherms move away from the origin at higher temperatures.

\*From standard gas equation, PV = RT. As T is constant, therefore, PV = constant

# NOTE:

• In an isothermal change, T = constant;  $\Delta T = 0$ 

As 
$$c = \frac{\Delta Q}{m(\Delta T)}$$
  
therefore,  $c = \infty$ 

i.e., during an isothermal change, specific heat of gas is infinite.

 For an ideal gas in an isothermal process, there is no change in internal energy of the gas, i.e., dU = 0. This is because T = constant, i.e., dT = 0.

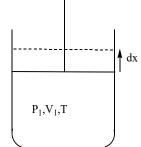
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### Work done in an isothermal expansion

Consider one gram mole of an ideal gas enclosed in a cylinder with perfectly conducting walls and fitted with a perfectly frictionless and conducting piston, Fig. Let  $P_1, V_1, T$  be the initial pressure, volume and temperature of the gas. Let the gas expand to a volume  $V_2$ , when pressure reduces to  $P_2$ . The temperature remains constant at T as equivalent amount of heat spent in expansion is gained from the surroundings. At any instant during expansion, let the pressure of the gas be P.

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If A is area of cross section of the piston, then force exerted by the gas on the piston is  $F = P \times A$ .



If we assume that pressure of the gas during an infinitestimally small outward displacement dx of the piston remains constant, then small amount of work done during expansion

$$\mathrm{dW} = \mathrm{F} \times \mathrm{d}x = \mathrm{P} \times \mathrm{A} \times \mathrm{d}x$$

dW = P (dV) where dV = A (dx) = small increase in volume of the gas.

Total work done by the gas in expansion from initial volume  $V_1$  to final volume  $V_2$  is  $W = \int_{V_2}^{V_2} P(dV)$ 

From standard gas equation,

$$PV = RT \quad \text{or} \quad P = RT/V$$

$$W = \int_{V_1}^{V_2} \frac{RT}{V} dV = RT \int_{V_1}^{V_2} \frac{1}{V} dV$$

$$= RT [\log_e V]_{V_1}^{V_2}$$

$$W = RT[\log_e V_2 - \log_e V_1] = RT \log_e \frac{V_2}{V_1}.$$

$$W = 2.3026 RT \log_{10} \frac{V_2}{V_1}$$
As
$$P_1 V_1 = P_2 V_2 \quad \therefore \quad \frac{V_2}{V_1} = \frac{P_1}{P_2}$$

$$W = 2.3026 RT \log_2 P_1$$

W = 2.3026 RT  $\log_{10} \frac{1}{P_2}$ Amount of heat spent in isothermal expansion

(in calories) is

$$H = \frac{W}{J} = 2.3026 \frac{RT}{J} \log_{10} \left( \frac{V_2}{V_1} \right)$$

This much heat must have been gained by the gas from the surroundings. THat is why temperature of the gas remains constant at T.

## 11.4.3 ADIABATIC OPERATION/CHANGE

A change in pressure and volume of a gas when no heat is allowed to enter into or escape from the gas is called an adiabatic change. Obviously, temperature

of gas will also change in adiabatic operations.

When a gas in an enclosure is compressed suddenly, some heat is produced. If this heat is not allowed to escape, the temperature of the gas would rise. Further, if the gas is allowed to expand suddenly, some of heat energy is spent in increasing the volume of the gas. If this heat is not compensated from the surroundings, the temperature of the gas would fall.

Obviously, for an adiabatic change, the exchange of heat between the gas and the surroundings must be prevented.

Hence, the two essential conditions for a perfect adiabatic change are :

(i) the walls of the container must be perfectly non-conducting in order to prevent any exchange of heat between the gas and its surroundings, and

(ii) the process of compression or expansion should be sudden so that there is no time for the exchange of heat.

Both these conditions are difficult to be realised strictly in practice. Therefore, perfect adiabatic changes are practically impossible.

Some examples of nearly perfect adiabatic changes

- 1. Sudden compression or expansion of a gas in a container with perfectly non conducting walls.
- 2. Sudden bursting of the tube of a bicycle tyre,
- 3. Propagation of sound waves in air and other gases,
- 4. Expansion of steam in the cylinder of a steam engine,
- 5. Expansion of hot gases in an internal combustion engine.

A curve which represents relative variations of pressure and volume of a given mass of a gas for an adiabatic change is called an adiabatic curve. The shape of adiabatic curves is similar to the shape of isothermal curves, Fig.

The adiabatic relation between P and V for a perfect gas is

 $PV^{\gamma} = K$ , a constant ...(2)

where,  $\gamma = \frac{\text{specific heat of the gas at constant pressure}}{\text{specific heat of the gas at constant volume}}$ 

Equation (2) can be rewritten as

$$\mathbf{P}_{1}\mathbf{V}_{1}^{\gamma}=\mathbf{P}_{2}\mathbf{V}_{2}^{\gamma}$$

From standard gas equation

PV = RT or P = RT/V

Putting in (2), we get

 $\frac{RT}{V}V^{\gamma} = K$   $T V^{(\gamma-1)} = \frac{K}{R} \text{ another constant.}$   $V^{(\gamma-1)} = \text{constant} \qquad \dots(4)$ or  $T_{1}V_{1}^{(\gamma-1)} = T_{2}V_{2}^{(\gamma-1)} \qquad \dots(5)$   $T_{1}V_{1}^{(\gamma-1)} = T_{2}V_{2}^{(\gamma-1)} \qquad \dots(5)$ 

This is the adiabatic relation between P and T

for a perfect gas. Again, from standard gas equation V = RT/P

Putting in (2), we get

$$P \frac{R^{\gamma} T^{\gamma}}{P^{\gamma}} = K$$

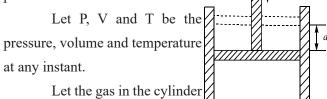
$$P^{(\gamma-1)} T^{\gamma} = \frac{K}{R^{\gamma}} \text{ another constant.}$$
i.e.,
$$P^{(\gamma-1)} T^{\gamma} = \text{ constant.}$$
or
$$P_{1}^{(\gamma-1)} T_{1}^{\gamma} = P_{2}^{(\gamma-1)} T_{2}^{\gamma}$$
There is the two products of the second second

This is the adiabatic relation between P and T for a perfect gas.

# 11.4.4 Relations between P, V and T in an Adiabatic process:

### (i) Relation between P and V

Consider one mole of an ideal gas contained in a thermally insulated cylinder fitted with a frictionless, movable and thermally insulated piston.



be compressed adiabatically so that the piston moves inwards through an infinitesimally small distance "dx".

If "A" is the area of the piston, the force acting on the piston F = PA.

Work done 
$$dW =$$
 Force X distance

 $dW = P.A.dx = P.dV \qquad \dots (1)$ 

where dV is decrease in volume = A.dx

The heat generated due to compression causes a rise in temperature dT. This heat energy is equal to  $C_v dT$ , where  $C_v$  is molar specific heat of the gas at constant volume. THis is equal to the change in internal energy dU.

$$dU = C_y dT \qquad \dots (2)$$

In an adiabatic process, there is no exchange of

$$dQ = 0 \qquad \dots (3)$$

Accdring to first law of thermodynamics dO = dU + dW

Substituting the values from (1), (2), & (3) in above equation

$$O = C_{v}.dT + P,dV \qquad \dots (4)$$

From the ideal gas equation, we have PV = RT.

On differentiating both sides

$$P.dV + V.dP = R.dT$$
  $dT = \frac{PdV + VdP}{R}$ 

Substituting the above value in equation (4),

we have

heat.

....

$$C_{v}\left(\frac{PdV + VdP}{R}\right) + PdV = 0$$

$$C_{v}(PdV + VdP) + RPdV = 0$$

$$C_{v}(PdV + VdP) + (C_{p} - C_{v})PdV = 0$$
(But C<sub>p</sub> - C<sub>v</sub> = R)

 $C_v P dV + C_v V dP + C_p P dV - C_v P dV = 0$ 

dividing the above equation throughout by

$$(C_v PV)$$
, we get

$$\frac{\mathrm{dP}}{\mathrm{P}} + \frac{\mathrm{C}_{\mathrm{P}}}{\mathrm{C}_{\mathrm{v}}} \frac{\mathrm{dV}}{\mathrm{V}} = 0$$

$$\frac{\mathrm{dP}_{\mathrm{n}}}{\mathrm{P}} + \gamma \frac{\mathrm{dV}}{\mathrm{V}} = 0 \qquad \left[ \because \gamma = \frac{\mathrm{C}_{\mathrm{p}}}{\mathrm{C}_{\mathrm{v}}} \right]$$

Let the initial pressure and volume br  $P_i$  and  $V_i$ respectively and the final pressure and volume be  $P_f$  and  $V_f$  respectively. Then on integration with in the limits,

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But

....

....

or

$$\begin{split} & \int_{V_i}^{V_f} \gamma \frac{dV}{V} = -\int_{P_i}^{P_f} \frac{dP}{P} \\ & \gamma [\log_e V]_{V_f}^{V_f} = [\log_e P]_{P_i}^{P_f} \\ & \gamma \log_e \left(\frac{V_f}{V_i}\right) = \log_e \left(\frac{P_f}{P_i}\right) \\ & \log_e \left(\frac{\frac{V_f}{P_i} P_f}{P_i P_i} \frac{P_f}{P_i}\right)^{\gamma} = \log_e \left(\frac{P_f}{P_i}\right) \\ & \therefore \frac{V_f^{\gamma}}{V_i^{\gamma}} = \frac{P_i}{P_f} \qquad \therefore P_i V_i^{\gamma} = P_f V_f^{\gamma} \\ & PV^{\gamma} = Constant. \qquad ...(5) \end{split}$$

This is the relation between P and V during an adiabatic process.

### (ii) Relation between V and T

From the gas equation PV = RT and P = RT/vSubstituting this value in equation

 $PV^{\gamma} = Constant$  $\left(\frac{\mathbf{RT}}{\mathbf{V}}\right)\mathbf{V}^{\gamma} = \mathbf{Constant}$ ...  $(V)^{\gamma-1} = \text{Constant}$  $TV^{\gamma - 1} = Constant$ ....

This is the relation between V and T during and adiabatic process.

#### Work done in an adiabatic change

Consider one mole of an ideal gas contained in a cylinder having non conducting walls and provided with a non conducting and frictionless piston. Let the pressure, and volume of the gas be P and V at any instant. Suppose the piston moves through an infinitesimally small distance 'dx' at constant pressure 'P'.

The work done dW = P.A.dx = P.dV

Where 'A' is the area of the piston and dV is the infinitesimally small change in volume.

The system changes from the initial state  $(P_1,$  $V_1$ ) to the final state ( $P_2$ ,  $V_2$ ). The temperature changes from  $T_1$  to  $T_2$ .

The work done during the change

$$W = \int dW = \int_{V_1}^{V_2} P.dV$$

For an adiabatic change

$$PV^{\gamma} = k (a \text{ constant})$$
  $P = \frac{K}{V^{\gamma}} = KV^{-\gamma}$ 

$$\therefore \qquad W_{adia} = \int_{V_1}^{V_2} KV^{\gamma} dv$$

$$W_{adia} = \int_{V_1}^{V_2} V^{\gamma} dv = K = \int_{V_1}^{V_2} KV^{\gamma} dv$$

$$W_{adia} = \frac{K}{1 - \gamma} [V_2^{1 - \gamma} - V_1^{1 - \gamma}]$$

$$W_{adia} = \frac{1}{1 - \gamma} [KV_2^{1 - \gamma} - KV_1^{1 - \gamma}]$$
But
$$P_1 V_1^{\gamma} = P_2 V_2^{\gamma}$$

$$\therefore \qquad W_{adia} = \frac{1}{1 - \gamma} [P_2 V_2^{\gamma} V_2^{1 - \gamma} = P_1 V_1^{\gamma} V_1^{1 - \gamma}]$$

$$W_{adia} = \frac{1}{1 - \gamma} [P_2 V_2 - P_1 V_1]$$
But from gas equation
$$P_1 V_1 = RT_1 \text{ and } P_2 V_2 = RT_2$$

$$\therefore \qquad W_{adia} = \frac{1}{1 - \gamma} (RT_2 - RT_1)$$

$$W_{adia} = \frac{R}{1 - \gamma} [T_2 - T_1]$$
$$W_{adia} = \frac{R}{\gamma - 1} [T_1 - T_2]$$

This expression gives the work done for a 1

mole of gas.

For 'n' moles of gas  

$$W_{adia} = \frac{nR}{\gamma - 1} (T_1 - T_2)$$

If 'm' is the mass of gas considered and M is its molecular weight then

$$W_{adia} = \frac{mR}{M(\gamma - 1)} (T_1 - T_2)$$

Work done if 1 gram of gas is considered

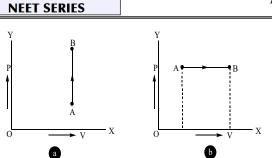
$$W_{adia} = \frac{R}{M(\gamma - 1)} (T_1 - T_2)$$

But R/M = r, the specific gas constant.

$$\therefore \qquad W_{adia} = \frac{r}{\gamma - 1} (T_1 - T_2)$$

# 11.4.5 ISOCHORIC AND ISOBARIC PROCESSES:

In an isochoric process, volume V is constant. No work is done on or by the gas. Heat absorbed by the gas goes entirely to change its internal energy and its temperature. The change in temperature for a given amount of heat is determined by specific heat of the gas at constant volume.



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The pressure-volume plot for an isochoric process is a vertical straight line parallel to pressure axis as shown in Fig(a). No work is done one or by the gas (i.e., W = 0). The area under the vertical line is zero. Heat absorbed changes directly the internal energy or temperature of the gas.

For an isobaric process, pressure-volume plot is a horizontal straight line parallel to volume axis as shown in Fig. (b).

In an isobaric process, pressure P is fixed. Work done by the gas is

 $W = P(V_2 - V_1) = \mu R(T_2 - T_1)$ = area ABCDA

As temperature changes, so does the internal energy of the gas.

The heat absorbed increases partially the internal energy and is spent partially in doing work. The change in temperature for a given amount of heat is determined by the specific heat of the gas at constant pressure.

# 11.4.6 Limitations of the first law of Thermodynamics

The first law of thermodynamics establishes the essential equivalence between the heat energy and mechanical work and says that the two can be converted into eachother. Further, 4.18 joule of mechanical work are required o produce one calorie of heat and viceversa. However, this law has the following limitations : 1. The first law does not indicate the direction in which the change can occur

For example (i) when two bodies at different temperatures are put in thermal contact with each other, heat flows from the body at higher temperature to the body at lower temperature. We now know that heat cannot flow from the body at lower temperature to the body at higher temperature, although first law of thermodynamics is not violated, (ii) When a moving car is stopped by applying brakes, work done against friction is converted into heat. When the car cools down, it does not start moving with the conversion of all its heat energy into mechanical work, (iii) When a bullet strikes a target, kinetic energy of the bullet is converted into heat energy. But heat energy developed in the target cannot be converted back into mechanical energy of the bullet enabling it to fly back.

2. The first law gives no idea about the extent of change

Our observations and experience tell that there appears to be no restriction on conversion of mechanical work into heat. But there are severe restrictions on the reverse process, i.e., conversion of heat energy into mechanical energy.

We know that heat is not converted into mechanical energy all by itself. An external agency called the heat engine is required for the purpose.

No heat engine can convert all the heat energy received from the source into mechanical energy. The first law of thermodynamics is silent about all this.

3. The first law of thermodynamics gives no information about the source of heat, i.e., whether it is a hot or a cold body.

#### 11.5.1 CYCLIC AND NON-CYCLIC PROCESSES

A cyclic process consists of a series of changes which return the system back to its initial state.

**For example,** suppose a system consists of a gas at pressure P, volume V and temperature T. Let the system be subjected to a number of changes including isothermal and adiabatic expansions and compressions. In the final state, if the system has the same pressure P, the same volume V and the same temperature T, the succession of changes involved are said to form a cyclic process.

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When the system is restored to its initial state, no intrinsic property of the system - including its internal energy can change, i.e., dU = 0. According to first law of thermodynamics, dQ = dU + dW = dW, i.e., net work done during the process = net amount of heat energy transferred. Internal energy of the system remains unchanged.

On the contrary, in a non-cyclic process, the series of changes involved do not return the system back to its initial state.

# 11.5.2 WORK DONE DURING A NON-CYCLIC PROCESS

Work done in a non-cyclic process is calculated in Art 8.10. It is equal to the area under the curve on the PV diagram.

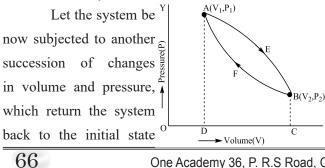
Conventionally, the work done is taken as positive, when the gas is expanding, and it is taken as negative, when the gas is compressed.

As the two points representing the initial and final state of a system can be joined by any number of j different curves, and the area enclosed by each curve is different, therefore in such cases, work done will be j different. Hence we conclude that the work done in a non cyclic process depends upon the path chosen or | the series of changes involved.

#### 11.5.3 WORK DONE DURING A CYCLIC PROCESS

Let A  $(V_1, P_1)$  represent the initial state of a gas, Fig. Let it be subjected to a number of changes in volume and pressure such that it acquires-the final state B ( $V_2$ ,  $P_2$ ), via the path AEB.

Work done by the gas in going from A to B, .... along AEB is  $W_1$  = area AEBCDA.



A  $(V_1, P_1)$ , along the path BFA. The total number of changes involved obviously constitute a cyclic process. .... Work done on the gas in going from B to A via

the path BFA is  $W_2 = -$  area BFADCB

Net work done by the gas in the cyclic process

 $W_{A \rightarrow B \rightarrow A} = W_1 + W_2 = area AEBCDA - area BFADCB$ = area AEBFA

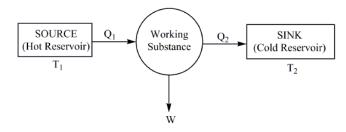
Hence, we conclude that work done per cycle is numerically equal to the area enclosed by the loop representing the cycle.

In Fig., cyclic path has been traced in the clockwise direction. The expansion curve AEB lies above the compression curve BFA. The area enclosed by the loop AEBFA comes out to be positive, indicating that net work is done by the system.

If cyclic path were traced in the anticlockwise direction, the expansion curve would be below the compression curve. The area of the loop would come out to be negative, indicating that net work will be done on the system.

### 11.5.4 HEAT ENGINE

A heat engine is a device which converts heat energy into mechanical energy. For this, a system is made to undergo a cyclic process.



A heat engine essentially consists of three parts :

- 1. Source of heat at higher temperature,
- 2. Working substance,
- 3. Sink of heat at lower temperature.

In a steam engine, steam acts as the working substance. In a diesel engine, a mixture of fuel vapours and air acts as the working substance. Heat is supplied to working substance at a relatively high input

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temperature from a place called the source/hot reservoir. It then undergoes a cyclic change consisting of several processes. It actually does the work. The remaining of input heat is ejected to the sink/cold reservoir.

The work done by the working substance of the system in a cycle, is transferred to the environment via some arrangement. For example, when the working substance is in a cylinder with moving piston, the piston transfers mechanical energy to the wheels of a vehicle via a shaft. The cycle is repeated again and again to obtain the desired useful work for some purpose.

Suppose,  $Q_1$  = amount of heat absorbed by the working substance from the source at  $T_1K$ , in one complete cycle, Fig.

 $Q_2$  = amount of heat rejected to the sink at  $T_2K$ , in the cycle.

W = net amount of external work done by the working substance, on the environment in the cycle.

... Net amount of heat absorbed in one cycle,

 $dQ = Q_1 - Q_2$ 

As the working substance returns to its initial state, the change in its internal energy = 0 i.e.,dU = 0According to first law of thermo – dynamics,

 $dQ = dU + dW \quad \therefore \quad dQ = dW$ 

i.e., net amount of heat absorbed = external work done by the engine

or  $Q_1 - Q_2 = W$ 

**Thermal efficiency** of a heat engine is defined as the ratio of net work done per cycle by the engine to the total amount of heat absorbed per cycle by the working substance from the source. It is denoted by  $\eta$ . Thus,

$$\eta = \frac{\text{Network done/cycle(W)}}{\text{Total amount of heat absorbed/cycle(Q_1)}} = \frac{Q_1 - Q_2}{Q_1}$$
$$\eta = 1 - \frac{Q_2}{Q_1}$$

As some heat is always rejected to the sink,  $Q_2 \neq 0$ . Therefore, efficiency is always less than 1, i.e., thermal efficiency of a heat engine is always less than 100%. For  $Q_2 = 0$ ,  $\eta = 1 = 100\%$ , i.e., the engine will have 100% efficiency in converting heat into work. Thus, first law of thermodynamics does not rule out a heat engine with 100% efficiency. However, practical experience shows that efficiency is less than 100% even if we eliminate all sorts of losses associated with actual heat engines.

It turns out that there is a fundamental limit on the efficiency of a heat engine set by an independent principle of nature, called the second law of thermodynamics.

#### Types of heat engines

In practice, heat engines are of two types :

1. External combustion engine, in which heat is produced by burning the fuel in a chamber outside the main body (i.e., cylinder and piston arrangement) of the engine.

For example, steam engine is an external combustion engine.

The theoretical value of efficiency of steam engine at 20 atmosphere pressure and 250°C is about 32%. However, practically thermal efficiency of a steam engine varies from 12% to 16%.

2. Internal combustion engine, in which heat is produced by burning the fuel inside the main body of the engine. Petrol engine and diesel engine are internal combustion engines. They are also called four stroke engines.

The theoretical value of thermal efficiency of an internal combustion engine is about 52 %.

Practically, efficiency of a petrol engine is about 26 % and the efficiency of a diesel engine is about 40%.

As petrol engine is light in weight and small in size, it is used in aeroplanes, cars, scooters etc.

A diesel engine is heavy and hence it is used in heavy vehicles like bus, truck, tractor, railway engine, etc.

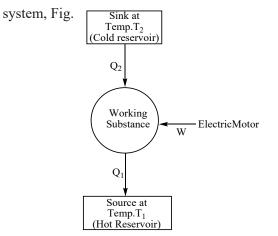
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# 11.5.5 PRINCIPLE OF A REFRIGERATOR (OR HEAT PUMP)

A refrigerator, as we all know, is a device used far cooling things. It is also called a heat pump.

As is known, the natural tendency of heat is to flow from higher temperature to lower temperature. However, if energy is supplied, heat can be made to flow from lower to higher temperatures, against its natural tendency. Refrigerators, air conditioners and heat pumps do just that.

An ideal refrigerator can be regarded as a heat engine working in the reverse direction. Thus, in a refrigerator, the working substance would absorb a certain quantity of heat Q<sub>2</sub> from the sink at lower temperature  $T_2$  and reject a larger amount of heat  $Q_1$  to the source at higher temperature  $T_1$  with the help of an external agency supplying the necessary energy to the



In a refrigerator, the working substance (usually, in gaseous form) goes through the following steps :

(a) Sudden expansion of the gas from high pressure to low pressure, resulting in cooling of the gas converting it into a vapour- liquid mixture.

(b) This mixture absorbs heat from the region to be cooled and gets converted into vapours.

(c) The vapours get heated on account of external work done on the system by the supply of electric power to the refrigerator.

(d) The heated vapours then release the heat to

the surroundings, bringing them to the initial state after completing one cycle.

Note that water and other food stuff to be cooled in the refrigerator serve as sink at lower temperature. The source in this case is the atmosphere or surrounding air at room temperature T<sub>1</sub>

In the cycle of changes, as the working substance returns to its initial state, therefore, there is no change in its internal energy, i.e., dU = 0.

If  $Q_2$  = amount of heat extracted per cycle from the cold reservoir at lower temperature T<sub>2</sub>, Fig.

W = Work done/cycle on the system-the refrigerant.

 $Q_1$  = amount of heat released/cycle to the source (surrounding air at higher temperature  $T_1$ ), then net amount of heat absorbed,  $dQ = Q_2 - Q_1$ 

Work done on the system dW = -W

According to first law of thermodynamics,

$$dQ = dU + dW$$

 $Q_2 - Q_1 = 0 - W$  or  $W = Q_1 - Q_2$ (\*)

Coefficient of performance of a refrigerator ( $\beta$ ) is defined as the ratio of quantity of heat removed per cycle from the contents of the refrigerator  $(Q_2)$  to the energy spent per cycle (W) to remove this heat. i.e.,

 $\beta = \frac{Q_2}{W}$ 

using (\*)

$$\beta = \frac{Q_2}{Q_1 - Q_2}$$

$$\beta = \frac{Q_2}{Q_1}$$

$$\beta = \frac{Q_2}{Q_1}}{\frac{Q_1}{Q_1} - \frac{Q_2}{Q_1}} = \frac{\frac{Q_2}{Q_1}}{1 - \frac{Q_2}{Q_1}}$$

In a Carnot cycle,  $\frac{Q_2}{Q_1} = \frac{T_2}{T_1} \qquad \therefore \beta = \frac{\frac{T_2}{T_1}}{1 - \frac{T_2}{T_1}} \dots (*1)$ or  $\beta = \frac{T_2}{T_1 - T_2} \dots \dots (1)$ 

.....(1)

This relation shows that to have large coefficient of performance of refrigerator,  $(T_1 - T_2)$ should be small, i.e., the object to be cooled must have

or

temperature close to the temperature of surroundings (/i.e., room temperature) before placing it in the refrigerator.

If  $\eta$  is efficiency of Carnot cycle, then

$$1 - \frac{T_2}{T_1} = \eta \qquad \therefore 1 - \eta = \frac{T_2}{T_1}$$
  
From (\*1),  $\beta = \frac{1 - \eta}{\eta}$ 

- Coefficient of performance of a refrigerator stands for efficiency of the refrigerator. Thus, higher the value of p, more efficient is the refrigerator.
- 2. Eqn.(1) shows that smaller is the value of  $(T_1-T_2)$ , greater is the value of  $\beta$ , i.e., smaller is the difference in temperatures of atmosphere and food stuff to be cooled, more efficient will be the refrigerator.

As the refrigerator works,  $T_2$  goes on decreasing due to formation of ice.  $T_1$  is almost constant. Therefore,  $\beta$  decreases. When the refrigerator is defrosted,  $T_2$ increases and hence  $\beta$  increases. Thus, defrosting is necessary for better working of the refrigerator.

3. A refrigerator cannot work without some external work done on the system, i.e., W is never zero. Hence,  $\beta = Q_2/W$  cannot be infinite i.e., coefficient of performance of a refrigerator can never be infinite.

#### **11.5.6 SECOND LAW OF THERMODYNAMICS**

We know that first law of thermodynamics is the principle of conservation of energy. A critical study shows that there are many conceivable processes that are perfectly allowed by the first law and yet they are never observed in practice. For example, the first law does not prohibit heat flowing from a cold body to a hot body. Still, when a hot body is placed in contact with a cold body, hot body has never been observed to become hotter and the cold body colder. Heat flows spontaneously from hot body to cold body.

Again, first law of thermodynamics does not prohibit a heat engine to convert 100% of heat energy into mechanical energy with no waste heat. But Carnot found that even an ideal heat engine would generate some waste heat. The real engines would generate even more waste heat.

Clearly, some additional basic principle of nature forbids certain phenomena, even though the first law is not violated. This principle which disallows certain phenomena consistent with the First Law of thermodynamics is known as the Second law of Thermodynamics, According to second law of thermodynamics, heat flows spontaneously from a substance at higher temperature to another at lower temperature. Heat does not flow spontaneously in the reverse direction.

The other two important forms of second law of thermodynamics are

#### (a) Kelvin Planck Statement

It is impossible to construct a heat engine which would absorb heat from a reservoir and convert 100% of the heat absorbed into work.

The law implies that a perfect heat engine with 100% efficiency can never be constructed. Infact, presence of sink is essential for continuous conversion of heat into work. If temperature of source  $T_1$  were equal to temperature of sink  $T_2$ , the efficiency of heat engine  $\left(\eta = 1 - \frac{T_2}{T_1}\right)$  becomes zero.

# (b) Clausius Statement

It is impossible to design a self acting machine unaided by any external agency, which would transfer heat from a body at a lower temperature to another body at a higher temperature.

We know that in a refrigerator, the working substance extracts heat from a colder body (sink) and rejects a larger amount of heat to a hotter body (source) with the help of an external agency, i.e., the electric supply to the refrigerator. No refrigerator can ever work without external supply of electric energy to it.

Both the statements of second law of thermodynamics are equivalent, as one can be obtained from the other.

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Note that the statements of second law start from 'it is impossible'. Thus, the second law is negative in form. Hence, it cannot be proved directly. However, the law is accepted universally and has been applied to a wide variety of phenomena like transfer of heat, expansion of a gas, diffusion of gases, etc.

## Note:

The second law of thermodynamics puts a fundamental limitation on

(i) efficiency of a heat engine,

(ii) coefficient of performance of a refrigerator.

The law emphasises that efficiency of a heat engine can never be 100%. It implies that heat released to the cold reservoir (/. e., sink) can never be made zero.

For refrigerator, the second law emphasises that its coefficient of performance can never be infinite. It implies that some external work has to be done to transfer heat from lower temperature to higher temperature.

# 11.5.7 REVERSIBLE AND IRREVERSIBLE PROCESSES

A thermodynamical process taking a system from initial state i to final state f is reversible, if the process can be turned back such that both, the system and the surroundings return to their original states, with no other change anywhere else in the universe.

For a process to be reversible, the following conditions must be satisfied :

1. The process should proceed at an extremely slow rate, i.e., process is quasi-static so that the system is in equilibrium with surroundings at every stage, i.e.,

(i) the system remains in mechanical equilibrium, i.e., there is no unbalanced force, (ii) the system remains in thermal equilibrium, i.e., all parts of the system and the surroundings remain at the same temperature, (iii) the system remains in chemical equilibrium, i.e., the internal structure of the system does not change.

2. The system should be free from dissipative

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forces like friction, inelasticity, viscosity, etc. This is because energy spent against such forces cannot be recovered.

As all the conditions mentioned above are of an idealized nature, no process in nature is truly reversible.

Infact, reversibility is an idealized concept which can never be attained. It can at best be approximated.

Some of the examples of approximately reversible processes are :

(i) An ideal gas allowed to expand slowly and then compressed slowly in a cylinder fitted with frictionless movable piston.

(ii) Electrolysis can be taken as a reversible process provided resistance offered by electrolyte is zero.

(iii) Slow compression and expansion of a spring can also be treated as a reversible process.

A process, which does not satisfy even one of the conditions for reversible process is called an irreversible process.

Infact, all spontaneous processes of nature are irreversible processes. For example, transfer of heat from a hot body to a cold body, ordinary expansion of a gas, diffusion of gases, stopping of a moving body through friction etc. are all irreversible processes.

## Irreversibility arises mainly from two causes :

(i) Many processes like free expansion or an explosive chemical reaction take the system to non equilibrium states, (ii) most processes involve friction, viscosity and other dissipative effects.

As the dissipative effects are present everywhere, and they can be minimised only and cannot be fully eliminated, therefore, most processes we deal with are irreversible processes.

Some additional examples of irreversible processes are :

(i) Production of heat on passing an electric current through a wire. The same amount of heat is produced

in a given time, even when the direction of current is reversed.

(ii) Most of the chemical reactions are irreversible, because they involve changes in the internal structure of the constituents.

(iii) The decay of organic matter is an irreversible process.

(iv) Rusting of iron is an irreversible process.

(v) Adiabatic (sudden) compression and expansion of a gas are irreversible processes.

(vi) Mixing of two different substances like water and alcohol.

(vii) The formation of solution of a solid in water etc.

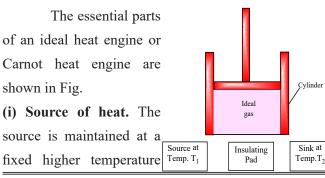
The significance of the concept of reversibility can be understood as follows :

The main concern of thermodynamics is the efficiency with which heat can be converted into mechanical work. The second law of thermodynamics ruled out the possibility of a perfect heat engine with 100% efficiency. It turned out that a heat engine based on idealised reversible processes achieves the highest possible efficiency. All other engines involving irreversibility of some kind have much lower efficiency. Therefore, reversibility is an important concept in thermodynamics.

#### 11.5.8 CARNOT CYCLE

Sadi Carnot devised an ideal cycle of operation for a heat engine, in the year 1824. This cycle came to be known as Carnot cycle. The machine used for realising this ideal cycle of operation is called an ideal heat engine or Carnot heat engine.

#### Construction



 $T_1$ , from which the working substance draws heat. The source is supposed to possess infinite thermal capacity and as such any amount of heat can be drawn from it without changing its temperature.

(ii) Sink of heat. The sink is maintained at a fixed lower temperature  $T_2$ , to which any amount of heat can be rejected by the working substance. It has also infinite thermal capacity and as such its temperature remains constant at  $T_2$ , even when any amount of heat is rejected to it.

(iii) Working substance. A perfect gas acts as the working substance. It is contained in a cylinder with non-conducting sides but having a perfectly conducting-base. This cylinder is fitted with perfectly non-conducting and frictionless piston.

Apart from these essential parts, there is a perfectly insulating stand or pad on which the cylinder can be placed. It would isolate the working substance completely from the surroundings. Hence, the gas can undergo adiabatic changes.

### Theory

The Carnot cycle consists of the following four stages :

1. Isothermal expansion,

2. Adiabatic expansion,

3. Isothermal compression,

4. Adiabatic compression.

The cycle is carried out with the help of the Carnot engine as detailed below:

Consider one gram mole of an ideal gas enclosed in the cylinder. Let  $V_1, P_1, T_1$  be the initial state of the gas. The initial state of the o gas is represented by the  $V_1, P_1, T_1 = V_1 = V_2, P_2$ 

point A on P - V diagram, Fig. We shall assume that all the four processes are quasi-staticand non dissipative,

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the two conditions for their reversibility. Now, the four processes are :

#### **1. Isothermal expansion**

Let the cylinder be placed on the source and the gas be allowed to expand by slow outward motion of the piston. Since it absorbs the requisite amount of heat from the source through the conducting base of the cylinder, therefore, temperature of the gas remains constant. This operation is called isothermal expansion and is represented by the isothermal curve AB. Let the amount of heat energy absorbed in the process be  $Q_1$ and  $W_1$  be the corresponding amount of work done by the gas in expanding isothermally from A ( $V_1$ ,  $P_1$ ) to B ( $V_2$ ,  $P_1$ )

$$\therefore \qquad Q_1 = W_1 = \int_{V_1}^{V_2} P.dV = RT_1 \log_e \frac{V_2^*}{V_1}$$
$$= \text{area ABMKA} \qquad \dots(1)$$

Note:

In an ideal heat engine, all processes are reversible and there occurs absolutely no wastage of energy due to friction and turbulence, etc.

#### 2. Adiabatic Expansion

The cylinder is now removed from the source and is placed on the perfectly insulating pad. The gas is allowed to expand further from B ( $V_2$ ,  $P_2$ ) to C ( $V_3$ ,  $P_3$ ). Since, the gas is thermally insulated from all sides, no heat can be gained from the surroundings. Temperature of gas falls to  $T_2$ , the expansion is adiabatic and is represented by the adiabatic curve BC. Let  $W_2$  be the work done by the gas in expanding adiabatically from B ( $V_2$ ,  $P_2$ ) to C ( $V_3$ ,  $P_3$ )

...  

$$W_{2} = \int_{V_{2}}^{V_{3}} \frac{P}{P} dV = \frac{R(T_{2} - T_{1})^{*}}{(1 - \gamma)} = \text{area BCNMB} \quad ...(2)$$
3. Isothermal Compression

The cylinder is now removed from the insulating pad and is placed on the sink at a temperature  $T_2$ . The piston is moved inwards slowly so that the gas

is compressed until its pressure is  $P_4$  and volume is  $V_4$ . This state is represented by the point D. Since, the base of cylinder is conducting, heat produced in compression will pass to the sink so that the temperature of the gas remains constant at  $T_2$ . This process is, therefore, isothermal and is represented by an isothermal curve, CD. Let  $Q_2$  be the amount of heat energy rejected to the sink and  $W_3$  be the amount of work done on the gas in compressing it isothermally from a state C ( $V_3$ ,  $P_3$ ) to D ( $V_4$ ,  $P_4$ ).

$$\therefore Q_2 = W_3 = \int_{V_3} -P.dV = -RT_2 \log_e \frac{V_4}{V_3} = RT_2 \log_e \frac{V_3}{V_4}$$
$$= -\operatorname{area CDLNC} \qquad \dots (3)$$

# 4. Adiabatic Compression

The cylinder is again placed on the insulating pad. The piston is further moved downwards so that the gas is compressed to its initial volume  $V_1$  and pressure  $P_1$ . As the gas is insulated from all sides, heat produced raises the temperature of the gas to  $T_1$ . This change is adiabatic and is represented by the adiabatic curve DA. Let  $W_4$  be the work done on the gas in compressing it adiabatically from a state D ( $V_4$ ,  $P_4$ ) to the initial state A ( $V_4$ ,  $P_1$ )

$$W_{4} = \int_{V_{4}}^{V_{1}} P \cdot dV = \frac{-R(T_{2} - T_{1})^{*}}{(1 - \gamma)}$$
$$= - \operatorname{area DAKLD} \qquad \dots (4)$$

Work done by the engine per cycle:

Total work done by the gas (in steps 1 and 2) =  $W_1 + W_2$ Total work done on the gas (in steps 3 and 4) =  $W_3 + W_4$  $\therefore$  Net work (W) done by the gas in a complete cycle,  $W = W_1 + W_2 - (W_3 + W_4)$  ....(5) From,  $W_2 = W_4$ , in magnitude,\*\*  $\therefore W = W_1 - W_3$  $W = Q_1 - Q_2$  ....(6)

In terms of area, we can rewrite as

W = area ABMKA + area BCNMB – area CDLNC – area DAKLD

$$W = area ABCDA \qquad \dots (7)$$

Hence, in Carnot heat engine, net work done by the gas per cycle is numerically equal to the area of the loop representing the cycle.

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### **EFFICIENCY OF CARNOT ENGINE**

Efficiency of Carnot engine is defined as the ratio of net mechanical work done per cycle by the gas (W) to the amount of heat energy absorbed per cycle from the source  $(Q_1)$ 

i.e., 
$$\eta = \frac{W}{Q_1}$$
 Using, (6)  
 $\eta = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$  ....(8)

Referring to Fig., as A  $(V_1, P_1)$  and B  $(V_2, P_2)$  lie on the same isothermal,

$$P_1V_1 = P_2V_2$$
 ....(9)

As B  $(V_2, P_2)$  and C  $(V_3, P_3)$  lie on the same adiabatic,

$$\therefore \qquad P_2 V_2^{\gamma} = P_3 V_3^{\gamma} \qquad \dots (10)$$

 $P_{3}V_{3} = P_{4}V_{4}$ 

Again, C ( $V_3$ ,  $P_3$ ) and D ( $V_4$ ,  $P_4$ ) lie on the same isothermal,

...

Finally, 
$$D(V_4, P_4)$$
 and  $A(V_1, P_1)$  lie on the same

....(10)

adiabatic,

$$\begin{array}{cccc} & & P_{4}V_{4}^{\gamma} = P_{1}V_{1}^{\gamma} & \dots(11) \\ \text{Multiplying (8), (9), (10) and (11), we get} \\ & (P_{1}V_{1})(P_{2}V_{2}^{\gamma})(P_{3}V_{3})(P_{4}V_{4}^{\gamma}) = \\ & & (P_{2}V_{2})(P_{3}V_{3}^{\gamma})(P_{4}V_{4})(P_{1}V_{1}^{\gamma}) \\ & V_{1}^{\gamma}V_{2}^{\gamma}V_{3}^{\gamma}V_{4}^{\gamma} = V_{1}^{\gamma}V_{2}V_{3}^{\gamma}V_{4} \\ & V_{2}^{\gamma-1}V_{4}^{\gamma-1} = V_{1}^{\gamma-1}V_{3}^{\gamma-1} \text{ or } (V_{2}V_{4})^{\gamma-1} = (V_{1}V_{3})^{\gamma-1} \\ & \text{or } & V_{2}V_{4} = V_{1}V_{3}, \quad \text{i.e., } \frac{V_{2}}{V_{1}} = \frac{V_{3}}{V_{4}} \\ & \text{os that} & \log \frac{V_{2}}{V_{1}} = \log \frac{V_{3}}{V_{4}} & \dots(12) \end{array}$$

Dividing(3) by (1), we get,

$$\frac{Q_2}{Q_1} = \frac{RT_2 \log_e V_3 / V_4}{RT_1 \log_e V_2 / V_1} = \frac{T_2}{T_1} \text{ i.e., } \frac{Q_2}{Q_1} = \frac{T_2}{T_1} \quad ...(13)$$

Putting this value in (7), we get, n

$$1 = 1 - \frac{T_2}{T_1}$$
 ....(14)

1. Eqn(14) reveals that efficiency of Carnot heat engine depends on temperature of source T<sub>1</sub>, and temperature of sink T<sub>2</sub>. But the efficiency does not depend upon the nature of the working substance.

2. As RHS of eqn.(14) is less than 1, therefore efficiency of Carnot heat engine is less than 100%.

3. For  $\eta = 1$  (i.e., 100 %), either  $T_1 = \infty$  or  $T_2 = 0$  K.

As source at infinite temperature or sink at 0K are not attainable, Carnot heat engine cannot have 100% efficiency.

If  $T_2 = T_1$  then from (14),  $\eta = 1 - \frac{T_1}{T_1} = 1 - 1 = 0$ 

i.e., the Carnot engine shall not work. Heme, it is not possible to convert heat energy into mechanical work unless source and sink of heat are at different temperatures.

5. From eqn.(13), we find that

$$\frac{Q_2}{Q_1} = \frac{T_2}{T_1} \qquad ...(15)$$
  
When  $T_2 \neq 0, Q_2 \neq 0$ 

i.e., some heat must be rejected to the sink. Heme efficiency of even an ideal heat engine can never be 100 %.

## The same thing can be understood as follows :

If heat is not rejected to the sink, the same will be retained by the working substance. Therefore, temperature of working substance will go on increasing and would ultimately become equal to temperature of the source. There will be no transfer of heat energy from the source to the working substance and hence the engine will stop working.

6. Note that Carnot engine is a reversible engine. Therefore, each step of Carnot cycle can be reversed. This will amount to taking heat  $Q_2$  from the cold reservoir (the sink) at lower temp. T<sub>2</sub>, doing work W on the system and transferring heat Q1 to the hot reservoir (the source at higher temp.  $T_1$ ). This is what is done in a refrigerator/heat pump.

7. An ideal gas has a simple equation of state which allows us to calculate  $\eta$  of Carnot engine readily. That is why we use an ideal gas as the working substance in Carnot engine.

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4.

...

#### Problem

Carnot engine takes in a thousand kilo calories of heat from a reservoir at 627°C, and exhausts it to a sink at 27°C. How much work does it perform ? What is the efficiency of the engine ?

Sol. Herer,

$$\begin{split} Q_1 &= 1000 \text{ kcal} = 10^6 \text{ cal. } T_1 = 627^\circ \text{C} = 627 + \\ 273 &= 900 \text{ K}, \text{ } T_2 = 27^\circ \text{C} = 300 \text{ K} \text{ ; } \text{W} = ? \\ \text{As } \frac{Q_2}{Q_1} &= \frac{T_2}{T_1} \quad \therefore \quad \frac{T_2}{T_1} Q_1 = \frac{300}{900} \times 10^6 \text{ cals.} \\ &= \frac{1}{3} \times 10^6 \text{ cals} \end{split}$$

Work done/cycle W =  $Q_1 - Q_2 = 10^6 - \frac{1}{3} \times 10^6$ 

$$= \frac{2}{3} \times 10^{6} \text{ cals.} = \frac{2 \times 4.2}{3} \times 10^{6} \text{ J}$$
$$= 2.8 \times 10^{6} \text{ J}$$
T

Also, $\eta = 1 - \frac{T_2}{T_1} = 1 - \frac{300}{900} = \frac{2}{3} = \frac{2}{3} \times 100 = 66.67\%.$ 

# **11.5.9 CARNOT THEOREM**

According to this theorem,

(a) Working between two given temperatures,  $T_1$  of hot reservoir (the source) and  $T_1$  of cold reservoir (the sink), no engine can have efficiency more than that of the Carnot engine.

(b) The efficiency of the Carnot engine is independent of the nature of the working substance.

To prove the (a) part of the theorem, imagine a reversible Carnot engine R and an irreversible heat engine I. Working between the same source temp. Tx and same temp, of sink  $T_2$ , Fig.

Suppose the two engines are coupled in such a way that irreversible engine *I* acts like a heat engine and reversible carnot engine R acts like a refrigerator.

Let the engine *I*, in one full cycle absorb  $Q_1$  heat from the source, deliver work W' and release the balance  $(Q_1 - W')$  to the sink.

We arrange that the engine R returns the same heat  $Q_1$  to the source when work W is done on it in one full cycle. Therefore, it would take heat  $(Q_1 - W)$  from the sink as shown in Fig.

Suppose efficiency of reversible engine R is less than the efficiency of irreversible engine I, i.e.,  $\eta_R < \eta_I$ 

For a given 
$$Q_1$$
; W< W'  
 $(Q_1 - W) > (Q_1 - W')$ 

Thus, on the whole, the coupled I - R system extracts heat  $(Q_1 - W) - (Q_1 - W) = (W' - W)$  from the sink (cold reservoir) and delivers the same amount of work (W' - W) in one cycle without any change in the source or anywhere else. This is against Second Law of Thermodynamics.

Hence, the assertion  $\eta_R < \eta_I (\text{or} (\eta_I > \eta_R) \text{ is wrong.}$ Hence, working between two given temperatures, no engine can have efficiency greater than the efficiency of revervible Carnot engine. This proves part (a) of the carnot theorem.

We can build a similar argument to show that a reversible heat engine with one particular working substance cannot be more efficient than the engine using another working substance. Hence, the maximum efficiency of Carnot engine  $\left(\eta = 1 - \frac{T_2}{T_1}\right)$ is independent of nature of the working substance undergoing Carnot cycle of operations. Exercises – 1

First Law of Thermodynamics  $(\Delta Q = \Delta U + \Delta W)$ 

- 1. First law of thermodynamics is given by [1] dQ = dU + PdV [2]  $dQ = dU \times PdV$ [2] dQ = (dU + dV)P [4] dQ = PdU + dV
- The internal energy of an ideal gas depends upon

   [1] Specific volume
   [2] Pressure

[3] Temperature [4] Density

 In changing the state of thermodynamics from A to B state, the heat required is Q and the work done by the system is W. The change in its internal energy is

[1] Q + W	[2] Q – W
[3] Q	[4] Q - W/2

- 4. If a system undergoes contraction of volume then the work done by the system will be
  [1] Zero [2] Negligible
  [3] Negative [4] Positive
- 5. Identify the wrong statement
  - [1] For isothermal process,  $\Delta T = 0$ 
    - [2] For isochoric process,  $\Delta V = 0$
    - [3] For isobaric process,  $\Delta P = 0$
    - [4] For adiabatic process,  $\Delta Q = 0$
    - [5] For cyclic process,  $\Delta W = 0$
- 6. The first law of thermodynamics is concerned with the conservation of
   [1] Momentum
   [2] Energy

[1] Momentum	[2] Energy
[3] Mass	[4] Temperature

7. 0.100 mol of an ideal gas is heated from 10 to 20° C keeping its (a) volume constant (b) pressure constant. Let  $\Delta U_a$  and  $\Delta U_b$  denote the change in the internal energy of the gas due to process (a) and (b) respectively. Then which of the following shall be true

 $[1] \Delta U_{a} = \Delta U_{b}$   $[2] \Delta U_{a} > \Delta U_{b}$   $[3] \Delta U_{a} = \Delta U_{b}$   $[4] \Delta U_{a} = \Delta U_{b} = 0$ 

 The internal energy change in a system that has absorbed 2 Kcals of heat and done 500 J of work is

[1] 8900 J	[2] 6400 J
[3] 5400 J	[4] 7900 J

 A system is given 300 calories of heat and it does 600 joules of work. How much does the internal energy of the system change in this process (J = 4.18 joules/cal)

		· ·
[1] 6	54 joule	[2] 156.5 joule
[3] –	300 joule	[4] – 528.2 joule

10. If Q, E and W denote respectively the heat added, change in internal energy and the work done in a closed cycle process, then

- [1] E = 0 [2] Q = 0[3] W = 0 [4] Q = W = 0
- 11. The specific heat *c* of a solid at low temperature shows temperature dependence according to the relation  $c = DT^3$  where D is a constant and T is the temperature in kelvin. A piece of this solid of mass m kg is taken and its temperature is raised from 20 K to 30 K. The amount of the heat required in the process in energy units is [1] 5 x 10<sup>4</sup> Dm [2] (33/4) x 10<sup>4</sup> Dm [3] (65/4)x 10<sup>4</sup> Dm [4] (5/4) x 10<sup>4</sup> Dm
- 12. An ideal gas is made to go through a cyclic thermodynamical process in four steps. The amount of heat involved are  $Q_1 = 600 \text{ J}$ ,  $Q_2 = -400 \text{ J}$ ,  $Q_3 = -300 \text{ J}$  and  $Q_4 = 200 \text{ J}$  respectively. The corresponding work involved are  $W_1 = 300 \text{ J}$ ,  $W_2 = -200 \text{ J}$ ,  $W_3 = -150 \text{ J}$  and W4. What is the value of  $W_4$  [1] 50 J [2] 100 J

	[_] 1000
[3] 150 J	[4] 50J

13. A system performs work  $\Delta W$  when an amount of heat is  $\Delta Q$  added to the system, the corresponding change in the internal energy is  $\Delta U$ . A unique function of the initial and final states (irrespective of the mode of change) is [1]  $\Delta Q$  [2]  $\Delta W$ [3]  $\Delta U$  and  $\Delta Q$  [4]  $\Delta U$ .

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14.	A container of volume 1m <sup>3</sup> is divided into two equal compartments by a partition. One of			heat supplied in any process [4] Work done is state dependent but not path			
	these compartments contains an ideal gas at dependent						
	300 K. The other compartment is vacuum. The						
	-	ermally isolated from its	21.	A perfect gas co		-	-
	<b>e</b> 1	artition is removed and the		vacuum. If the o	•	-	y bursts, then
		by the whole volume of the		the temperature		0	
	container. Its tempera			[1] Remains con	nstant		omes zero
	[1] 300 K	[2] 239 K [4] 100 K		[3] Increases		[4] Dec	reases
	[3] 200 K	[4] 100 K	22.	When two bodi		d B are in	thermal
15.	110 I of heat is ad	ded to a gaseous system,	22.	equilibrium	cs A ai		l ulei illai
15.				[1] The kinetic	energi	es of all th	e molecules of
	-	se internal energy change is 40 J, then the unt of external work done is		A and B will be	-		
	[1] 150 J	[2] 70 J		[2] The potentia		vies of all	the molecules
	[1] 150 J [3] 110 J	[4] 40J		of A and B will	-	-	the morecules
				[3] The internal	-		wo bodies wil
16.	Which of the followin	ig is not a thermodynamical		be equal	0		
	function	e i			kineti	c energy of	f the molecules
	[1] Enthalpy	[2] Work done		of the two bodie			
	[3] Gibb's energy	[4] Internal energy					
			23.	If $\Delta Q$ and $\Delta W$ re	epresei	nt the heat	supplied to the
17.	When the amount of work done is 333 cal and change in internal energy is 167 cal, then the heat supplied is			system and th	e wor	k done c	on the system
				respectively, the		rstlawofth	ermodynamics
				can be written a			
	[1] 166 cal	[2] 333 cal		$[1] \Delta Q = \Delta U + $			
	[3] 500 cal	[4] 400 cal		$[3] \Delta Q = \Delta W - A$			$= -\Delta W - \Delta U$
1.0				where $\Delta U$ is the	e interr	al energy	
18.	First law of thermodynamics states that					0.1	1 . 1 . 0 . 1
	[1] System can do w		24.	For free expan		of the gas	which of the
	[2] System has temp			following is true		0	
	[3] System has press			[1] $Q = W = 0$ and $\Delta E_{int} = 0$			
	[4]Heat is a form of	energy		[2] $Q = 0$ , $W > 0$ and $\Delta E_{int} = -W$ [3] $W = 0$ , $Q > 0$ , and $\Delta E_{int} = Q$			
19.	A thermo dynamical	system is changed from		[3] W = 0, Q > [4] W > 0, Q < 0			
19.		$_{2}$ ) by two different process.		[4] W > 0, Q <		$\Delta L_{int} = 0$	
		will remain same will be	25.	Which of the fo	llowin	g can not	determine the
	[1] $\Delta Q$	[2] $\Delta W$	20.	state of a therm		0	
	$\begin{bmatrix} 1 \end{bmatrix} \Delta Q + \Delta W$	$[4] \Delta Q - \Delta W$		[1] Pressure and	•	-	1
				[2] Volume and			
20.	Which of the followi	ng statement is true		[3] Temperature	-		
	Which of the following statement is true [1] Internal energy of a gas depends only on the			[4] Any one of p	-		or temperature
	state of the gas.					,	1
	-	process change in internal	26.	Which of the fo	llowin	g is not a t	hermodynamic
	energy is maximum	-		co-ordinate	·		-
	[2] 4 1	ure, volume graph equals				[4] R	

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**NEET SERIES** 

	IE ACADEMY NEET SERIES	PHYS	ICS - VC	OL III C	LASS-XII THERMODYNAMICS
27.	In a given process f dQ < 0 Then for the [1] The temperature [2] The volume will [3] The pressure wi [4] The temperature	e will decrease l increase ll remain constant		that the gas molecule and 10 J of work is	changed in such a manner es gives out 20 J of heat done on the gas. If the of the gas was 40 J, then gy will be [2] 20 J [4] 40 J
28.	pressure is $C_p = 3$ constant volume is one kilogram hydrog to 20° C at constant	f hydrogen gas at constant 8.4 x 10 <sup>3</sup> cal/kg°C and at $C_v = 2.4 \times 10^3$ cal/kg°C. If gen gas in heated from 10° C pressure, the external work to maintain it at constant [2] 104 cal [4] 5 x 10 <sup>3</sup> cal	34.	internal energy is incr [1] Its temperature wi [2] Its temperature wi [3] Its temperature wi [4] None of these	ll increase ll decrease
29.		ving parameters does not rmodynamic state of matter [2] Temperature* [4] Work	36.	depend on path [1] Temperature [3] Work First law of thermodyn [1] Newton's law	<ul><li>[2] Energy</li><li>[4] None of these</li><li>namics is a special case of</li></ul>
30.	is ideal gas, its inter [1] Kinetic energy of [2] Kinetic and pote	ential energy		<ul><li>[1] Newton's law</li><li>[2] Law of conservation</li><li>[3] Charle's law</li><li>[4] Law of heat exchange</li></ul>	
31.	for any thermodyna [1] The internal ener [2]Internal energy ar [3] The change in er	wing statements is correct	37. 38.	at a constant pressure 0°C to 100°C . Then t energy is [1] 6.56 joules [3] 12.48 x 10 <sup>2</sup> joules If the ratio of specific	
32.	the first law of them [1] It introduces the energy [2] It introduces the	concept of the internal concept of the entropy ment of the principle of rgy	39.	the volume changes pressure p, is [1] $R/(\gamma - 1)$ [3] $pV/(\gamma - 1)$ If $C_v = 4.96$ cal/mo	[3] $\gamma p V/(\gamma - 1)$ ble K, then increase in remperature of 2 moles of
33.		ic process, pressure of a		[1] 27.80 cal [3] 13.90 cal	[2] 19.84 cal [4] 9.92 cal

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40. Temperature is a measurement of coldness or between the same two states in another process in which it absorbs 10<sup>5</sup> J of heat. Then in the hotness of an object. This definition is based on [1] Zeroth law of thermodynamics second process [2] First law of thermodynamics [1] Work done on the gas is  $0.5 \times 10^5 \text{ J}$ [3] Second law of thermodynamics [2] Work done by gas is  $0.5 \times 10^5 \text{ J}$ [4] Newton's law of cooling [3] Work done on gas is  $10^5$  J [4] Work done by gas is  $10^5$  J 41. When heat energy of 1500 joules, is supplied to a gas at constant pressure 2.1 x  $10^5$ N/m<sup>2</sup>, 47. During an isothermal expansion, a confined there was an increase in its volume equal to ideal gas does -150 J of work against its  $2.5 \times 10^{-3} \text{m}^3$ . The increase in internal energy surrounding. This implies that of the gas in joules is [1] 150 J of heat has been added to the gas [1] 450 [3] 975 [2] 150 J of heat has been removed from the gas [2] 525 [4] 2025 [3] 300 J of heat has been added to the gas 42. If heat given to a system is 6 kcal and work [4] No heat is transferred because the process is isothermal done is 6 kJ. Then change in internal energy is [2] 12.5 kJ [1] 19.1 kJ [3] 25 kJ [4] Zero 48. 100g of water is heated from 30°C to 50°C ignoring the slight expansion of the water, the 43. In a thermodynamics process, pressure of a change in its internal energy is (specific heat of fixed mass of a gas is changed in such a manner wafer is 4184 J/Kg/K) that the gas releases 20 J of heat and 8 J of work [1] 4.2 kJ [2] 8.4 kJ [4] 2.1 kJ is done on the gas. If the initial internal energy [3] 84 kJ of the gas was 30 J. The final internal energy When an ideal monoatomic gas is heated at will be 49. [1] 18 J [2] 9 J constant pressure, fraction of heat energy [3] 4.5 J [4]36 J supplied which increases the internal energy of gas, is 44. A monoatomic gas of n-moles is heated from [1] 2/5 [2] 3/5 [3] 3/7 [4] 3/4 temperature  $T_1$  to  $T_2$  under two different conditions (i) at constant volume and (ii) at 50. If the amount of heat given to a system is 35 J constant pressure. The change in internal and the amount of work done on the system is energy of the gas is 15 J, then the change in internal energy of the [1] More for (i) [2] More for (ii) system is [3] Same in both cases [1] – 50 J [3] 30 J [2] 20J [5] – 20 J [4] Independent of number of moles [4] 50J 45. The state of a thermodynamic system is **ISOTHERMAL PROCESS** represented by [1] Pressure only [2] Volume only [3] Pressure, volume and temperature [4] Number of moles 1. For an ideal gas, in an isothermal process [1] Heat content remains constant 46. A perfect gas goes from state A to another state [2] Heat content and temperature remain constant B by absorbing 8 x 10<sup>5</sup> J of heat and doing [3] Temperature remains constant 6.5 x 10<sup>5</sup>J of external work. It is now transferred [4] None of the above

	IE ACADEMY NEET SERIES	PHYS	ICS - VC	DL III	CI	ASS-XII THEF	RMODYNAMICS
2.	one mole of nitrogen	1163.4 joule is supplied to a gas, at room temperature then the rise in temperature is		[1] 1672.5 J [3] – 1728 J		[2] 1728 . [4] – 1572	
	(Given $R = 8.31 \text{ J m}$ [1] 54K[2] 2[4] 8K[4] 4	ole <sup>-1</sup> R <sup>-1</sup> ) 28K [3]65K	90	Work done in depends [1] Only on t	temperatu	re	-
3.	In an isothermal exp [1] Internal energy o [2] Internal energy o [3] Internal energy re	f the gas increases f the gas decreases		<ul><li>[2] Only on y</li><li>[3] On both t</li><li>expansion ra</li><li>[4] Only on i</li></ul>	the temper tio	ature and v	olume
		nergy of gas molecule	10.	Work done p [1] RT log <sub>10</sub> -			÷
4.	volume of 96 g of ox	versible expansion, if the xygen at 27°C is increased		[3] RT $\log_{e} \frac{N}{N}$	$\frac{V_2}{V_1}$	[4] RT log	$g_e \frac{V_1}{V_2}$
	by the gas will be	litres, then the work done	11.	The isotherm at pressure P	is		-
	[1] 300 R log <sub>10</sub> 2 [3] 900 R log <sub>10</sub> 2	$\begin{bmatrix} 2 \end{bmatrix} & 81 \text{ R } \log_{e} 2 \\ \begin{bmatrix} 4 \end{bmatrix} & 2.3 \text{ x } 900 \text{ R } \log_{10} 2 \end{bmatrix}$	10		2] γP		[4] P/γ
5.	pressure is connected volume 3 litres. The	5 litres of a gas at 0.8 m d to an evacuated vessel of e resultant pressure inside nole system to be isolated) [2] 0.5 m [4] 3/4 m	12.	During an iso [1] Its intern [2] Its intern [3] The work quantity of h [4] Both (b)	al energy al energy done by eat absorb	decreases does not cha the gas is ec bed by it	ange
6.	expansion from a sta entropy $\Delta S$ (i $\rightarrow f$ ) is [1] 0	bes a reversible isothermal te i to <i>f</i> . The change in [2] >0	13.	The isotherm normal press [1] 1.013 x 1 [3] 1.013 x 1	oure is 0 <sup>5</sup> N/m <sup>2</sup>	[2] 1.013	
7.	<ul><li>[3] &lt;0</li><li>[4] Not defined for th</li><li>The gas law PV/T =</li></ul>	•	14.	In an isother [1] Boyle's la [3] Gaylussa	aw	[2] Charle	•
/.	<ul><li>[1] Isothermal chang</li><li>[2] Adiabatic change</li><li>[3] Both isothermal a</li></ul>	es only	15.	wrong [1] Temperature is constant [2] Internal energy is constant			ment is
8.	22.4 litres at 0°C and	having a volume equal to 1 atmospheric pressure in		[3] No excha [4] (a) and (b	-		
	-	nally so that its volume s. The work done in this	16.	volumesino	eased from	Vto2Vund	B have their erisothermal ernal energy
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	NEET SERIES	PHYSICS	S - VOL III		CLASS- XII THERMODYNAMICS
	[1] Will be same in I	both A and B		$[1] 3.6 \times 10^3$ cal of he	at flowed out from the gas
	[2] Will be zero in b	oth the gases		[2] 3.6 x 10 <sup>3</sup> cal of he	eat flowed into the gas
	[3] Of B will be mor				eat flowed into the gas
	[4] Of A will be mor				at flowed out from the gas
17.	The specific heat of	f a gas in an isothermal	24.	-	a gas in an isothermal
	process is			change, the result wil	l be
	[1] Infinite	[2] Zero		[1] External work dor	
	[3] Negative	[4] Remains constant		[2] Rise in temperatu	
				[3] Increase in interna	•••
18.	A thermally insulate	d container is divided into		[4] External work do	ne and also rise in temp.
	two parts by a scree	n. In one part the pressure			
	and temperature are	P and T for an ideal gas	25.	When 1 g of water	at 0°C and 1 x 10 <sup>5</sup> N/m <sup>2</sup>
		part it is vacuum. If now a		*	into ice of volume 1.091
		ed in the screen, then the		cm <sup>3</sup> , the external wor	k done will be
	temperature of the g			[1] 0.0091 joule	[2] 0.0182 joule
	[1] Decrease	[2] Increase		[3] – 0.0091 joule	[4] – 0.0182 joule
	[3] Remain same	[4] None of the above			
			26.	-	porisation of water is 2240
19.		s the occurrence of an		•	n the process of expansion
	isothermal process s			-	crease in internal energy is
	[1] Copper	[2] Glass		[1] 2408 J	[2] 2240 J
	[3] Wood	[4] Cloth		[3] 2072 J	[4] 1904 J
20.	In an isothermal pro-	cess the volume of an ideal	27.		onvert 1 cubic centimeter
	gas is halved. One c	•			to 1671 cubic centimeter
		f the system decreases			C at a pressure of one
	[2] Work done by th			-	e work done against the
	[3] Work done by th	0 0		atmospheric pressure	•
	[4] Internal energy o	f the system increases		[1] 540 cal	[2] 40 cal
				[3] Zero cal	[4] 500 cal
21.	• •	ocess in which temperature	• •	~	
	•	ains constant though other	28.	One mole of an ideal gas expands at a c	
	variable P and V ma			-	from an initial volume of
	[1] Isochoric process				time of 20 litres. The work $P = 8.21$ l/m ala K)
	[3] Isobaric process	[4] None of these			gasis(R=8.31 J/mole-K)
22	If an ideal ago is ago	an use of is otherwoodly, then		[1] 750 joules	[2] 1728 joules
22.	-	npressed isothermally then		[3] 1500 joules	[4] 3456 joules
	<ul><li>[1] No work is done against gas</li><li>[2] Heat is released by the gas</li></ul>		29.	A aulindar fitted wi	th a piston contains 0.2
		gy of gas will increase	29.	•	rature 27°C. The piston is
	[4] Pressure does no			-	the air within the cylinder
		i unange			l equilibrium with the
23.	When an ideal gas in	a cylinder was compressed			e approximate work done
<i></i> .	-	ston, the work done on the		-	final volume is twice the
		e 1.5 x $10^4$ joules . During		initial volume	
	this process about	I.J.A. IO JOUICS . During			
	ans process about				

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	[1] 543 J	[2] 345 J		[3] 40/3
	[3] 453 J	[4] 600 J		[4] 32 times its initial pressure
30.		leal gas is 1 litre and its		The pressure and density of a diatomic gas
		2 cm of mercury column.		$(\gamma = 7/5)$ change adiabatically from (P, d) to
	-	s is made 900 cm <sup>3</sup> by		(P', d'). If $d'/d = 32$ , then P'/P should be
	· •	ermally. The stress of the		[1] 1/128 [2] 32 [2] 128 [4] Norma (4) - 1 - 1
	gas will be	$\begin{bmatrix} 2 \end{bmatrix} 7$ and $\begin{pmatrix} \mathbf{m} \\ \mathbf{m} \\ \mathbf{m} \end{pmatrix}$		[3] 128 [4] None of the above
	[1] 8 cm (mercury) [3] 6 cm (mercury)	[2] 7 cm (mercury) [4] 4 cm (mercury)	8.	An ideal gas at 27°C is compressed adiabatically
		[4] 4 cm (mercury)	0.	to 8/27 of its original volume. If $\gamma = 5/3$ , then the rise in temperature is
	ADIABATIC	PROCESS		[1] 450 K [2] 375 K
	ADIADATIC .	I ROCESS		[3] 225 K [4] 405 K
1.	During an adiabatic r	process, the pressure of a		
		portional to the cube of its	9.	Two identical samples of a gas are allowed to
	absolute temperature.		-	expand (i) isothermally (ii) adiabatically. Work
	[1] 1.3 [2] 2	[3] 1.7 [4] 1.5		done is
				[1] More in the isothermal process
2.	The work done in an	adiabatic change in a gas		[2] More in the adiabatic process
	depends only on			[3] Neither of them
	[1] Change is pressur	e [2] Change is volume		[4] Equal in both processes
	[3] Change in temper	ature		
	[4] None of the aboe.		10.	Which of the two, (i) compressing a gas
				isothermally until its volume is reduced by half
3.	In adiabatic expansio			(ii) compressing the same gas adiabatically
	$[1] \Delta U = 0$	$[2] \Delta U = negative$		until its volume is reduced by half, will require
	$[3] \Delta U = positive$	$[4] \Delta W = Zero.$		more work to be done
4		· · · · · · · · · · · · · · · · · · ·		[1] (i) [2] (ii)
4.		owing processes is the		[3] Both will require the same amount of work
	entropy change zero [1] Isobaric	[2] Isothermal		[4] It will depend upon the nature of the gas
	[3] Adiabatic	[4] None of the above	11.	The slopes of isothermal and adiabatic curves
			11.	are related as
5.	$1 \text{ mm}^3$ of a gas is con	npressed at 1 atmospheric		[1]Isothermalcurveslope=adiabaticcurveslope
5.	-	ture 27°C to 627°C. What		[2] Isothermal curve slope = $\gamma \times$ adiabatic curve
	• •	under adiabatic condition		slope
	( $\gamma$ for the gas = 1.5)			[3] Adiabatic curve slope = $\gamma \times \text{isothermal}$
	$[1] 27 \times 10^5 \text{ N/m}^2$	[2] 80 x 10 <sup>5</sup> N/m <sup>2</sup>		curve slope
	$[3] 36 \times 10^5 \text{ N/m}^2$	[4] 56 x $10^5$ N/m <sup>2</sup>		[4] Adiabatic curve slope = $1/2$ x isothermal
				curve slope
6.	A monoatomic gas (γ	= 5/3) is suddenly		
	compressed to 1/8 of	its original volume	12.	Pressure-temperature relationship for an ideal
	adiabatically, then the	e pressure of the gas will		gas undergoing adiabatic change is $(\gamma = C_p/C_v)$ [1] PT <sup><math>\gamma</math></sup> = constant [2] PT <sup>-1+<math>\gamma</math></sup> = constant
	change to			[1] $PT^{\gamma} = constant$ [2] $PT^{-1+\gamma} = constant$
	[1] 24/5	[2] 8		[3] $P^{\gamma-1}T^{\gamma} = \text{constant}$ [4] $P^{1-\gamma}T^{\gamma} = \text{constant}$

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CLASS- XII THERMODYNAMICS

- 13. Ideal gas undergoes an adiabatic change in its state from  $(P_1, V_1, T_1)$  to  $(P_2, V_2, T_2)$ . The work done (W) in the process is ( $\mu$  = number of moles,  $C_p$  and  $C_v$  are molar specific heats of gas) [1] W =  $\mu(T_1 - T_2)C_p$  [2] W =  $\mu(T_1 - T_2)C_v$ [1] W =  $\mu(T_1 + T_2)C_p$  [2] W =  $\mu(T_1 + T_2)C_v$
- 14. For a gas of non rigid diatomic molecules, the value of  $\gamma = C_p / C_v$  is [1] 9/7 [2] 7/5 [3] 5/3 [4] 11/9
- 15. A thermally insulated vessel contains an ideal gas of molecular mass M and ratio of specific heats  $\gamma$ . It is moving with speed v and is suddenly brought to rest. Assuming no heat is lost to the surroundings, its temperature increases by

[1] 
$$\frac{(\gamma - 1)}{2(\gamma + 1)R} \text{ Mv}^2$$
 [2]  $\frac{(\gamma - 1)}{2\gamma R} \text{ Mv}^2$   
[3]  $\frac{\gamma \text{Mv}^2}{2R}$  [4]  $\frac{(\gamma - 1)}{2R} \text{ Mv}^2$ 

- 16. If  $\gamma$  denotes the ratio of two specific heats of a gas, the ratio of slopes of adiabatic and isothermal PV curves at their point of intersection is
- 17. Air in a cylinder is suddenly compressed by a piston, which is then maintained at the same position. With the passage of time
  - [1] The pressure decreases
  - [2] The pressure increases
  - [3] The pressure remains the same
  - [4] The pressure may increase or decrease depending upon the nature of the gas
- 18. When a gas expands adiabatically
  - [1] No energy is required for expansion
  - [2] Energy is required and it comes from the
  - wall of the container of the gas
  - [3] Internal energy of the gas is used in doing work
  - [4] Law of conservation of energy does not hold

- 19. A thermos flask made of stainless steel contains several tiny lead shots. If the flask is quickly shaken, up and down several times, the temperature of lead shots
  [1] Increases by adiabatic process
  [2] Increases by isothermal process
  - [3] Decreases by adiabatic process
  - [4] Remains same
- 20. In changing the state of a gas adiabatically from an equilibrium state A to another equilibrium state B, an amount of work equal to 22.3 J is done on the system. If the gas is taken from state A to B via a process in which the net heat absorbed by the system is 9.35 calories, the net work done by the system in latter case will be [1159] [21169]

21. The adiabatic Bulk modulus of a perfect gas at pressure is given by

[1] P	[2] 2P
[3] P/2	[4] γ P

- 22. An adiabatic process occurs at constant[1] Temperature[2] Pressure[3] Heat
  - [4]Temperature and pressure
- 23. How many times a diatomic gas should be expanded adiabatically so as to reduce the root mean square velocity to half
  [1] 64 [2] 32 [3] 16 [4] 8.

24. For adiabatic processes  $\left(\gamma = \frac{C_p}{C_v}\right)$ [2]  $P^{\gamma}V = \text{constant}$  [2]  $T^{\gamma}V = \text{constant}$ [3]  $TV^{\gamma-1} = \text{constant}$  [4]  $TV^{\gamma} = \text{constant}$ 

25. An ideal gas is expanded adiabatically at an initial temperature of 300 K so that its volume is doubled. The final temperature of the hydrogen gas is ( $\gamma = 1.40$ ) [1] 227.36 K [2] 500.30 K [3] 454.76 K [4] - 47°C

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26.	the work done by the	rgoes a change in which system equals the decrease y. The system must have	33.	[1] 1280 J [3] 1815 J For adiabatic proc	[2] 1610 J [4] 2025 J ess, wrong statement is
	<ul><li>[1] Isothermal chang</li><li>[2] Adiabatic change</li><li>[3] Isobaric change</li><li>[4] Isochoric change</li></ul>			[1] dQ = 0 [3] Q = constant [4] Entropy is not	[2] dU = -dW
27.	gas, the internal en	expansion of 2 moles of a ergy was found to have The work done by the gas [2] 100 J [4]100 J	34.	adiabatically to volume. The temp will be [1] 10°C [3] 668K	tially at 18°C is compressed one-eighth of its original erature after compression [2] 887°C [4] 144° C
28.	final temperatures at then the change in in $[1] \frac{R}{\gamma - 1} (T_2 - T_1)$	nsion of a gas initial and re T <sub>1</sub> and T <sub>2</sub> respectively, ternal energy of the gas is $[2] \frac{R}{\gamma - 1} (T_1 - T_2)$ $[4] Zero$	35.	compressed to 0	a gas at STP is adiabatically .7 liter. Taking the initial $T_1$ , the work done in the [2] $\frac{3}{2}$ RT <sub>1</sub> [4] $\frac{9}{2}$ RT <sub>1</sub>
29.	suddenly compressed	a volume of 8 litres. It is d to a volume of 1 litre. he gas will be $[\gamma = 5/3]$ [2] 9327° C [4] 927° C	36.	the system is term [1] Isochoric	ich no heat enters or leaves ed as [2] Isobaric [4] Adiabatic
30.	compress one kilo m and in this process t increases by 7°C. The [1] Triatomic	is performed in order to nole of a gas adiabatically he temperature of the gas $e gas is (R = 8.3 \text{ J mol}^{-1} \text{ K}^{-1})$ noatomic and diatomic [4] Diatomic	37. 38.	occupies a volume adiabatically to th done by the gas wil [1] – 216123 J [3] 2500 J Adiabatic modulu	[4] - 2500  J is of elasticity of a gas is
31.	value of $\Delta P/P$ is equa	ansion of a perfect gas, the al to $[2] - \frac{\Delta V}{V}$ $[4] - \gamma^2 \frac{\Delta V}{V}$	20	modulus of elastic [1] 1.8 x 10 <sup>5</sup> N/m <sup>2</sup> [3] 1.4 x 10 <sup>5</sup> N/m <sup>2</sup>	[2] 1.5 x 10 <sup>5</sup> N/m <sup>2</sup> [4] 1.2 x 10 <sup>5</sup> N/m <sup>2</sup>
32.	compressed adiabation	ble of diatomic gas is cally to half of its volume,	39.	$\Delta U + \Delta W = 0$ is va [1] Adiabatic proc [3] Isobaric proces	ess [2] Isothermal process

 $\gamma = 1.41$ . The work done on gas will be

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47.

- 40. An ideal gas at a pressures of 1 atmosphere and temperature of 27° C is compressed adiabatically until its pressure becomes 8 times the initial pressure, then the final temperature is  $(\gamma = 3/2)$ [1] 627° C [2] 527° C
  - [3] 427° C [4] 327° C
- Air is filled in a motor tube at 27° C and at a 41. pressure of 8 atmospheres. The tube suddenly bursts, then temperature of air is [Given  $\gamma$  of air = 1.5] [1] 27.5° C [2] 75° K [3] 150° K [4] 150° C
- 42. If  $\gamma = 2.5$  and volume is equal to 1/8 times to the initial volume then pressure P' is equal to (Initial pressure = P) [1] P' = P[2] P'= 2P $[3] P' = P x (2)^{15/2}$ [4] P'= 7P
- 43. During an adiabatic expansion, the increase in volume is associated with which of the following possibilities w.r.t. pressure and temperature

Pressure	Temperature	
Increase	Increase	
Decrease	Decrease	
Increase	Decrease	
Decrease	Increase	
	Increase Decrease Increase	IncreaseIncreaseDecreaseDecreaseIncreaseDecrease

44. During an adiabatic process, the pressure of a gas is found to be proportional to the cube of its absolute temperature. The ratio  $C_p / C_v$  for the gas is

[1] 3/2	[2] 4/3
[3] 2	[4] 5/3.

- 45. In adiabatic expansion of a gas
  - [1] Its pressure increases
  - [2] Its temperature falls
  - [3] Its density increases
  - [4] Its thermal energy increases
- 46. One mole of an ideal gas at an initial temperature of T K does 6 R joules of work adiabatically. If

the ratio of specific heats of this gas at constant pressure and at constant volume is 5/3, the final temperature of gas will be

[1] (T + 2.4) K	[2] (T – 2.4)K
[3] (T + 4)K	[4](T-4)K

- One mole of an ideal gas with  $\gamma = 1.4$ , is adiabatically compressed so that its temperature rises from 27°C to 35°C. The change in the internal energy of the gas is (R = 8.3 J/mol.K)[1] – 166 J [2] 166 J [3] – 168 J [4] 168 J
- 48. A gas for which  $\gamma = 1.5$  is suddenly compressed to  $1/4^{th}$  of the initial volume. Then the ratio of the final to the initial pressure is [1] 1:16 [2] 1:8 [3] 1:4 [4] 8:1
- 49. The internal energy of the gas increases in [1] Adiabatic expansion [2] Adiabatic compression [3] Isothermal expansion [4] Isothermal compression
- 50. We consider a thermodynamic system. If  $\Delta U$ represents the increase in its internal energy and W the work done by the system, which of the following statements is true [1] AD = -W in an adiabatic process [2] AD = W in an isothermal process [3] AD = -W in an isothermal process [4] AD = W in an adiabatic process
- 51. Which property of the system does not change in an adiabatic process
  - [1] Volume [2] Temperature [3] Density [4] Total amount of heat

# **ISOBARIC AND ISOCHORIC PROCESSES**

1. A gas expands under constant pressure P from volume  $V_1$  to  $V_2$ . The work done by the gas is

[3]  $P(V_1^{\gamma} - V_2^{\gamma})$  [4]  $P\frac{V_1V_2}{V_2 - V_1}$ 

 $[1] P(V_2 - V_1)$ 

 $[2] P(V_2 - V_1)$ 

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2.	. When heat in given to a gas in an isob process, then [1] The work is done by the gas		8.	A gas expands $10^3 \text{ N/m}^2$ , the wo [1] 2.5 ergs	0.25m <sup>3</sup> at constant pressure rk done is [2] 250 J
	[2] Internal energy o [3] Both (1) and (2)			[3] 250 W	[4] 250 N
	[4] None from (1) an		9.	boiling at atmosp	is converted into steam by heric pressure. The volume
3.	In thermodynamic following statements	processes which of the is not true		changes from 2 x done by the system	10 m <sup>3</sup> to 3.34 m <sup>3</sup> . The work m is about
	[1] In an adiabatic pr insulated from the su	ocess the system is		[1] – 340 kJ [3] 170 kJ	[2] – 170 kJ [4] 340 kJ
	remains constant	process the temperature rocess $PV^{\gamma} = constant$	10.	heated at constan	s volume $V_0$ at 27° C. It is it pressure so that its volume e final temperature is [2] 32.6° C [4] 150 K
4.	contains some amou	-cylinder based enclosure int of gas at a pressure of is transferred to the gas at	11.	If 300 ml of a gas	s at 27° C is cooled to 7°C at , then its final volume will be
	400 kPa. Then heat is transferred to the gas at constant pressure in a quasi–static process. The piston moves up slowly through a height of 10 cm. If the piston has a cross-section area of 0.3			[1] 540 m <i>l</i> [4] 280 m <i>l</i>	[2] 350 m <i>l</i> [4] 135 m <i>l</i>
	m <sup>2</sup> , the work done b [1] 6 kJ [3] 7.5 kJ	the work done by the gas in this process is 12. 6 kJ [2] 12 kJ		If the temperature of 1 mole of ideal gas changed from 0°C to 100°C at consta pressure, then work done in the process (R = 8.3  J/Mole-Kelvin)	
5.	straight line parallel [1] Isothermal	[2] Isobaric		[1] 8.3 x 10 <sup>-3</sup> J [2] 8.3 x 10 <sup>2</sup> J	[2] 8.3 x 10 <sup>-2</sup> J [4] 8.3 x 10 <sup>3</sup> J
6	[3] Irreversible	[4] Adiabatic	13.	The amount of wo	xpands from volume $V_1$ to $V_2$ ork done by the gas is greatest
6.	of the system remain [1] Isobaric [3] Adiabatic	s, does the internal energy constant [2] Isothermal [4] Isochoric		when the expansi [1] Isothermal [3] Adiabatic	[2] Isobaric [4] Equal in all cases.
7.	completely changed	quid with volume $V_1$ is into a gas of volume $V_2$ at ressure P and temperature	14.	Which of the follo [1] Isothermal [3] Isobaric	owing is a slow process [2]Adiabatic [4] None of these
	T. If the latent heat of	f evaporation for the given e increase in the internal is	15.	volume of an id 2.4 x $10^{-4}$ m <sup>3</sup>	to be done in decreasing the deal gas by an amount of at normal temperature and pressure of 1 x 10 <sup>5</sup> N/m <sup>2</sup> [2] 27 J

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16.	temperature 27°C ha maintains at constan atm. The gas is con	g 1 mole of a gas at a as a movable piston which t pressure in container of 1 apressed until temperature work done is (C for gas is	3.	If the door of a refrigerator is kept open, then which of the following is true [1] Room is cooled [2] Room is heated [3] Room is either cooled or heated [4] Room is neither cooled nor heated
	[1] 703 J [3] 121 J	[2] 831 J [4] 2035 J	4.	If we consider solar system consisting of the earth and sun only as one of the ideal thermodynamic system. The sun works as
17.	In a reversible isoch [1] $\Delta W = 0$ [3] $\Delta T = 0$	bric change [2] $\Delta Q = 0$ [4] $\Delta U = 0$		source of energy having temperature 6000 K and the earth as sink having temperature 300K, the efficiency of solar system would be on the basis of exchange of radiations
18.	Which is incorrect [1] In an isobaric pro [2] In an isochoric p		5.	[1] 30% [2] 65% [3] 75% [4] 95% What is the value of sink temperature when
	[2] In an isothermal [3] In an isothermal [4] In an isothermal	process, $\Delta T = 0$	5.	efficiency of engine is 100 %         [1] 0 K       [2] 300 K         [3] 273 K       [4] 400 K
19.	Which relation is con [1] $\Delta Q = \Delta U$ [3] $\Delta Q = \Delta W$	rrect for isometric process [2] $\Delta W = \Delta U$ [4] None of these	6.	In a Carnot engine, the temperature of reservoir is 927°C and that of sink is 27°C. If the work done by the engine when it transfers heat from
20. 21.	In which thermody remains same [1] Isobaric [3] Adiabatic In an isochoric proce	ynamic process, volume [2] Isothermal [4] Isochoric ess if T.=27°C and		The engine when it transfers heat from reservoir to sink is $12.6 \times 10^6$ c/, the quantity of heat absorbed by the engine from the reservoir is [1] $16.8 \times 10^6$ J [2] $4 \times 10^6$ J [3] $7.6 \times 10^6$ J [4] $4.2 \times 10^6$ J [5] $20.8 \times 10^6$ J
	$T_2 = 127^{\circ}C$ , then $P_1/I$ [1] 9/59 [3] 3/4	P <sub>2</sub> will be equal to [2] 2/3 [4] None of these	7.	<ul><li>In a cyclic process, work done by the system is</li><li>[1] Zero</li><li>[2] Equal to heat given to the system</li><li>[3] More than the heat given to system</li><li>[4] Independent of heat given to the system</li></ul>
HEA		ERATOR AND SECOND		[4] independent of near given to the system
1.	600K has work output amount of heat energy from source per cycle [1] 1800 J/cycle	orking between 300K and at of 800 J per cycle. What is rgy supplied to the engine e [2] 1000 J/cycle	8.	A carnot engine, having an efficiency of $\eta = 1/10$ as heat engine, is used as a refrigerator. If the work done on the system is 10 J, the amount of energy absorbed from the reservoir at lower temperature is [1] 99 J [2] 90 J [3] 1 J [4] 100 J
2.		[4] 1600 J/cycle performance of a Carnot between 30°C and 0°C is [3] 9 [4] 0	9.	The change in the entropy of a 1 mole of an ideal gas which went through an isothermal process from an initial state $(P_1, V_1, T)$ to the final state $((P_2, V_2, T))$ is equal to

[1] Zero[2] R In T[1] 50%[2] 24%[3] 0.75%[5][3] R In $V_1V_2$ [4] R In $V_2V_1$ [3] R In $V_1V_2$ [4] R In $V_2V_1$ [3][5][5]10.Efficiency of Carnot engine is 100% if[1] $T_2 = 273$ K[2] $T_2 = 0$ K[3]		E ACADEMY NEET SERIES	PHYS	PHYSICS - VOL III			LASS- XII THERM	IODYNAMICS
10.Efficiency of Carnot engine is 100% if [1] $T_2 = 273 K$ [2] $T_1 = 0 K$ 17.A Carnot engine has efficiency 1/5. E becomes 1/3 when temperature of 		[1] Zero	[2] R In T		[1] 50% [2	2] 24%	[3] 0.75%	[4] 0.4%
<ol> <li>Efficiency of Carnot engine is 100% if [1] T<sub>2</sub> = 273 K [2] T<sub>2</sub> = 0 K [3] T<sub>1</sub> = 273 K [2] T<sub>3</sub> = 0 K [3] T<sub>1</sub> = 273 K [2] T<sub>3</sub> = 0 K [3] T<sub>1</sub> = 273 K [2] T<sub>3</sub> = 0 K [3] T<sub>1</sub> = 273 K [2] T<sub>1</sub> = 0 K [3] S0 K [2] 300 K [2] 300 K [3] S00 K [2] 300 J [4] T00 J [2] 300 J [5] S00 J [4] 700 J</li> <li>A Carnot engine absorbs an amount Q of heat from a reservoir at an absolute temperature of T3. The amount of heat rejected is 27°C. Efficiency of and the engine is 27°C. Efficiency of engine is 25%. Then temperature of sink of Carnot engine is 27°C. Efficiency of carnot's engine operating with an efficiency is τ<sub>1</sub>, and when T<sub>1</sub> = 0°C and T<sub>2</sub> = -200°C, Its efficiency is τ<sub>1</sub>, and when T<sub>1</sub> = 0°C and T<sub>2</sub> = -200°C, Its efficiency is τ<sub>1</sub>, and when T<sub>1</sub> = 0°C and T<sub>2</sub> = -200°C, Its efficiency is τ<sub>1</sub>, then what is η<sub>1</sub>/η<sub>5</sub> [1] 0.638 [4] Cannot be calculated 15. The efficiency of Carnot's engine operating with an efficiency is τ<sub>1</sub>, then what is η<sub>1</sub>/η<sub>5</sub> [1] 0.638 [4] Cannot be calculated 16. The efficiency of Carnot's engine between reservoirs, maintained at temperature 16. The efficiency of Carnot's engine between reservoirs, maintained at temperature 17. The temperature of carnot's engine operating with an efficiency is η<sub>1</sub> and when T<sub>1</sub> = 0°C and T<sub>2</sub> = -200°C, its efficiency is η<sub>1</sub> and when T<sub>1</sub> = 0°C and 18. The efficiency of Carnot's engine 19. The temperature of issink is 11] 300 K [2] 400 K 13. InaCarnotengine, when T<sub>2</sub> = 0°C and T<sub>1</sub> = 200°C, 14. The temperature of arcservoir of Carnot's engine operating with an efficiency is η<sub>1</sub> and when T<sub>1</sub> = 0°C and T<sub>2</sub> = -200°C, its efficiency is η<sub>1</sub> and when T<sub>1</sub> = 0°C and 10. Prevent radiation [2] Finit ideal 10. Carnot engine cannot give 100% cfficiency because we cannot 10. Prevent radiation [2] Finit ideal 10. Reach absolute zero temperature 10. Reach</li></ol>		$[3] R In V_1/V_2$	[4] R In $V_2/V_1$					
[1] $T_2 = 273 K$ [2] $T_3 = 0 K$ decreasedby 50K. What is the temperatur[3] $T_1 = 273 K$ [4] $T_1 = 0 K$ [1] $325 K$ [2] $375 K$ [3] $300 K$ [4] $350 K$ [3] $300 K$ [4] $350 K$ 11. A Carnot's engine used first an ideal monoatomic gas then an ideal diatomic gas. If the source and sink temperature are 411° C and 69 °C respectively and the engine extracts 1000 J of heat in each cycle, then area enclosed by the PV diagram isA measure of the degree of disorder of is known as[1] 100 J[2] 300 J[3] Enthalpy[4] Entropy[3] 500 J[4] 700 J[3] Enthalpy[4] Entropy[3] 500 J[4] 700 J[3] 846 K[4] 754 K[3] $Q/2$ [4] $Q/3$ [3] 846 K[4] 754 K[3] $Q/2$ [4] $Q/3$ [3] 846 K[4] 754 K[3] $Q/2$ [4] $Q/3$ [3] 1000 K[2] 960 K[3] $Q/2$ [4] $Q/3$ [3] 1000 K[2] 960 K[3] $Q/2$ [4] $Q/3$ [3] 11 is oscientist says that the efficiency of engine which operates at source tem[3] $Q/2$ [4] $Q/3$ [3] 11 is oscientist says that the efficiency of engine which operates at source tem[3] $Q/2$ [4] $Q/3$ [3] 11 is impossible[3] $127^{\circ}$ C[3] $127^{\circ}$ C[4] $127^{\circ}$ C[3] $127^{\circ}$ C[3] $127^{\circ}$ C[4] $100 K$ [3] $100 K$ [2] $400 K$ [3] Transfer of heat by conduction[3] $100 K$ [2] $400 K$ [3] $100 K$ [3] $100 K$ [2] $400 K$ [3] $100 K$ [3] $00 K$ [4] $100 K$ [2] $400 K$ <t< td=""><td></td><td></td><td></td><td>17.</td><td></td><td>-</td><td>•</td><td>•</td></t<>				17.		-	•	•
[3] $T_1 = 273 \text{ K}$ [4] $T_1 = 0 \text{ K}$ [1] $325 \text{ K}$ [2] $375 \text{ K}$ [3] $300 \text{ K}$ [4] $350 \text{ K}$ [3] $300 \text{ K}$ [4] $350 \text{ K}$ [3] $300 \text{ K}$ (4] $350 \text{ K}$ [3] $300 \text{ K}$ [4] $350 \text{ K}$ [3] $300 \text{ K}$ (2] $350 \text{ K}$ [3] $300 \text{ K}$ [4] $350 \text{ K}$ [1] $100 \text{ J}$ [2] $300 \text{ J}$ [3] $100 \text{ J}$ [3] $1100 \text{ J}$ [2] $300 \text{ J}$ [3] $500 \text{ J}$ [4] $700 \text{ J}$ [3] $1100 \text{ K}$ [2] $960 \text{ K}$ [1] $100 \text{ J}$ [2] $300 \text{ J}$ [3] $1000 \text{ K}$ [2] $960 \text{ K}$ [1] $100 \text{ J}$ [2] $300 \text{ J}$ [3] $1000 \text{ K}$ [2] $960 \text{ K}$ [1] $100 \text{ J}$ [2] $20/3$ [3] $846 \text{ K}$ [4] $754 \text{ K}$ and rejects heat to a sink at a temperature of[3] $846 \text{ K}$ [4] $754 \text{ K}$ and rejects heat to a sink at a temperature of[3] $123^{\circ}\text{C}$ [3] $22^{\circ}\text{C}$ [3] $2/2$ [4] $2Q/3$ [2] $20/3$ [3] $11 \text{ is quite probable}$ [3] $122^{\circ}\text{C}$ [3] $122^{\circ}\text{C}$ [3] $123^{\circ}\text{C}$ [4] $220^{\circ}\text{C}$ [3] $122^{\circ}\text{C}$ [3] $123^{\circ}\text{C}$ [4] $200 \text{ K}$ [3] $123^{\circ}\text{C}$ [4] $200 \text{ K}$ [2] $400 \text{ K}$ [3] $100 \text{ K}$ [2] $400 \text{ K}$ [3] $100 \text{ K}$ [3] $100 \text{ K}$ [4] $700 \text{ K}$ [2] $100 \text{ K}$ [3] $100 \text{ K}$ [2] $100 \text{ K}$ [2] $100 \text{ K}$ [3] $123^{\circ}\text{C}$ [3] $100 \text{ K}$ [2] $400 \text{ K}$ [3] $100 \text{ K}$ [2] $400 \text{ K}$ [3] $100 \text{ K}$ <trd>[3] <math>100 \text{ K}</math>[2] <math>100 </math></trd>	10.	Efficiency of Carn	ot engine is 100% if		becomes 1/	3 when	temperature	of sink is
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11.A Carnot's engine used first an ideal monoatomic gas then an ideal diatomic gas. If the source and sink temperature are 411° C and 69 °C respectively and the engine extracts 1000 J of heat in each cycle, then area enclosed by the PV diagram is [1] 100 J [2] 300 J [3] 500 J [4] 700 JA measure of the degree of disorder of is known as [1] Isobaric [2] Isotropy [3] Enthalpy [4] Entropy [3] Enthalpy [4] Entropy 		$[3] T_1 = 273 K$	$[4] T_1 = 0 K$		[1] 325 K		[2] 375 K	
gas then an ideal diatomic gas. If the source and sink temperature are 411° C and 69 °C respectively and the engine extracts 1000 J of heat in each cycle, then area enclosed by the PV diagram is [1] 100 J [2] 300 JA measure of the degree of disorder of is known as[1] 100 J [2] 300 J[3] Enthalpy[4] Entropy[3] 500 J[4] 700 J[3] Enthalpy[4] Entropy[1] 100 J [3] 500 J[4] 700 J[3] Enthalpy[4] Entropy[3] 500 J[4] 700 J[3] Enthalpy[4] Entropy[3] 0.05 K[2] 900 K[3] Enthalpy[4] Entropy[3] 0.42[4] 20 /3[3] 846 K[4] 754 K[3] 0.42[4] 20 /3[3] 846 K[4] 754 K[3] 0.42[4] 20 /3[3] 846 K[4] 754 K[3] 0.42[3] 0.43[3] 0.43[4] 20 /3[3] 0.43[3] 0.43[4] 20 /3[3] 11 1000 K[2] 960 K[3] 127°C[2] 20 /3[3] 11 15 is impossible[2] 11 is impossible[3] 127°C[3] 27°C[3] 27°C[3] 27°C[3] 1300 K[2] 400 K[3] Transfer of heat by conduction[4] 1300 K[2] 400 K[3] Transfer of heat by conduction[4] 1300 K[2] 400 K[3] 600 K[4] 800 K[5] 10.577[2] 0.733[3] 600 K[4] 800 K[6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperature23.[6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperature23.[6] The efficiency of Carnot's engine operating between reservoirs					[3] 300 K		[4] 350 K	
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respectively and the engine extracts 1000 J of heat in each cycle, then area enclosed by the PV diagram is [1] 100 J [2] 300 J [4] 700 J [3] 500 J [4] 700 J (3] 500 J [4] 700 J (3] 500 J [4] 700 J (4] Cannot engine absorbs an amount Q of heat from a reservoir at an absolute temperature T and rejects heat to a sink at a temperature of T/3. The amount of heat rejected is [1] Q /4 [2] Q /3 [3] Q /2 [4] 2Q /3 [3] 27°C [2] 327°C [3] 127°C [2] 327°C [3] 127°C [2] 327°C [3] 127°C [4] 27°C 21. Which of the following processes is re [1] Transfer of heat by radiation [2] Electrical heating of a nichrome w [3] Transfer of heat by radiation [2] Electrical heating of a nichrome w [3] Transfer of heat by conduction [4] Isothermal compression [1] 300 K [2] 400 K [3] 500 K [4] 700 K 22. Efficiency is $\eta_1$ and when $T_1 = 0°C$ and $T_2 = -200°C$ , its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ [4] Cannot be calculated [5] The efficiency of Carnot's engine operating with an efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ [4] Cannot be calculated [5] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures [6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures [6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures [6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures [6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures [6] Reserve tamperature of carnot's engine operating between reservoirs, maintained at temperatures [6] Reserve tamperature of Carnot's engine operating between reservoirs, maintained at temperatures [6] Reserve tamperature of Carnot's engine operating between reservoirs, maintained at temperatures [6] Reserve tamperature of carnot's engine operating between reservoirs, maintained at temperatures [6] Reserve tamperature of carnot's engine operating between reservoirs,		gas then an ideal	diatomic gas. If the source	18.	A measure of	f the degre	ee of disorder	of a system
heat in each cycle, then area enclosed by the PV diagram is[3] Enthalpy[4] Entropy[1] 100 J[2] 300 J[3][4] Entropy[3] 500 J[4] 700 JA carnot engine has the same e between 800 K to 500 K and x K to 60 value of x is[1] 100 J[2] 300 J[4] 700 J[2] A Carnot engine absorbs an amount Q of heat from a reservoir at an absolute temperature T and rejects heat to a sink at a temperature of T/3. The amount of heat rejected is [3] Q /2[4] 2Q /3[3] Q /2[4] 2Q /3[3] 846 K[4] 754 K[3] Q /2[4] 2Q /3[2] C[2] 11 is impossible[3] Q /2[4] 2Q /3[2] 11 is impossible[2] 11 is impossible[3] 27°C.[3] 127°C[2] 327°C[3] 127°C[3] 122°C[2] 327°C[3] 127°C[2] 327°C[3] 122°C[4] 27°C[2] 327°C[3] 11 is quite probable[4] Data is incomplete[4] Data is incomplete[4] Data is incomplete[1] 300 K[2] 400 K[3] Transfer of heat by conduction [4] Isothermal compression[4] In a Carnotengine, when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, its efficiency is $\eta_2$ , then what is $\eta_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_1$ [1] 0.577[3] 0.638[4] Cannot be calculated23.[4] Cannot be calculated23.[5] The efficiency of Carnot's engine between reservoirs, maintained at temperatures[6] The efficiency of Carnot's engine between reservoirs, maintained at temperatures[2] Find ideal [3] Reach absolute zero temperature		and sink temperat	ture are 411° C and 69 °C		is known as			
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[3] 500 J[4] 700 Jbetween 800 K to 500 K and x K to 60 value of x is12.A Carnot engine absorbs an amount Q of heat from a reservoir at an absolute temperature T and rejects heat to a sink at a temperature of T/3. The amount of heat rejected is [1] Q/4[2] Q/313.The temperature of sink of Carnot engine is $27^{\circ}$ C. Efficiency of engine is 25%. Then temperature of source is [1] 227°C[2] 327°C13.The temperature of source is [1] 227°C[2] 327°C[3] 127°C[4] 27°C[2] 327°C[3] 300 K[2] 400 K[3] 500 K[4] 700 K[2][3] 500 K[4] 700 K[3] 500 K[4] 700 K[3] 500 K[4] 700 K[3] 0.638[4] Cannot be calculated[4] Cannot be calculated23.[5.The efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ [1] 0.577[6.The efficiency of Carnot's engine between reservoirs, maintained at temperature[6.The efficiency of Carnot's engine operating between reservoirs, maintained at temperature		•	e, then area enclosed by the		[3] Enthalpy		[4] Entropy	Į
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12.A Carnot engine absorbs an amount Q of heat from a reservoir at an absolute temperature T and rejects heat to a sink at a temperature of T/3. The amount of heat rejected is [1] Q/4 [2] Q/3 [3] Q/2[1] 1000 K [2] 960 K [3] 846 K[4] 754 K13.The temperature of sink of Carnot engine is 27°C. Efficiency of engine is 25%. Then temperature of source is [1] 227°C20.A scientist says that the efficiency of engine which operates at source tem 127°C and sink temperature 27°C is 2 [3] 127°C14.The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of is sink is [1] 300 K [3] 500 K[2] 400 K [3] 500 K21.15.InaCarnotengine, when $T_2 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ [3] 0.638 [4] Cannot be calculated23.Efficiency of a Carnot engine cannot give 100% efficiency because we cannot [1] Prevent radiation16.The efficiency of Carnot's engine between reservoirs, maintained at temperatures23.Even Carnot engine cannot give 100% efficiency because we cannot [1] Prevent radiation		[3] 500 J	[4] 700 J		between 800	K to 500	K and $x$ K to	600 K. The
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T/3. The amount of heat rejected is20.A scientist says that the efficiency of $[1] Q/4$ $[2] Q/3$ $[3] Q/2$ $[4] 2Q/3$ 13. The temperature of sink of Carnot engine is $27^{\circ}C$ and sink temperature $27^{\circ}C$ is 2 $[1] 27^{\circ}C$ $[2] 327^{\circ}C$ $[3] 127^{\circ}C$ $[2] 327^{\circ}C$ $[3] 127^{\circ}C$ $[2] 327^{\circ}C$ $[3] 127^{\circ}C$ $[4] 27^{\circ}C$ $[3] 127^{\circ}C$ $[2] 327^{\circ}C$ $[3] 127^{\circ}C$ $[4] 27^{\circ}C$ $[1] 227^{\circ}C$ $[2] 327^{\circ}C$ $[3] 127^{\circ}C$ $[4] 27^{\circ}C$ $[1] 27^{\circ}C$ $[2] 327^{\circ}C$ $[3] 127^{\circ}C$ $[4] 27^{\circ}C$ $[1] 20^{\circ}C$ $[4] 20^{\circ}C$ $[1] 300 K$ $[2] 400 K$ $[3] 500 K$ $[4] 700 K$ $[3] 500 K$ $[4] 700 K$ $[3] 500 K$ $[4] 700 K$ $[3] 0.538$ $[4] Cannot be calculated$ $[4] Cannot be calculated$ $[2] 0.733$ $[3] 0.638$ $[4] Cannot be calculated$ $[4] Cannot be calculated$ $[3] Reach absolute zero temperature[3] Reach absolute zero temperature[3] Reach absolute zero temperature$		from a reservoir a	t an absolute temperature T		[3] 846 K		[4] 754 K	
[1] $Q/4$ [2] $Q/3$ engine which operates at source term[3] $Q/2$ [4] $2Q/3$ engine which operates at source term[3] $Q/2$ [4] $2Q/3$ [1] $27^{\circ}C$ and sink temperature $27^{\circ}C$ is 2[1] $27^{\circ}C$ [2] $327^{\circ}C$ [3] $127^{\circ}C$ [4] $27^{\circ}C$ [3] $127^{\circ}C$ [4] $27^{\circ}C$ [4] $27^{\circ}C$ [4] $21$ are pobable[4] $27^{\circ}C$ [2] $327^{\circ}C$ [3] $127^{\circ}C$ [4] $27^{\circ}C$ [3] $127^{\circ}C$ [4] $27^{\circ}C$ [4] $27^{\circ}C$ [4] $21$ ti si possible but less probable[4] $27^{\circ}C$ [4] $27^{\circ}C$ [4] $27^{\circ}C$ [3] $11$ ti si quite probable[4] $127^{\circ}C$ [4] $27^{\circ}C$ [4] $27^{\circ}C$ [4] $21$ ti si possible but less probable[3] $127^{\circ}C$ [4] $27^{\circ}C$ [4] $27^{\circ}C$ [4] $21$ ti si possible but less probable[3] $127^{\circ}C$ [4] $27^{\circ}C$ [4] $27^{\circ}C$ [4] $21$ ti si quite probable[4] $120^{\circ}K$ [5] $110^{\circ}K$ [6] $11^{\circ}C$ and the efficiency of $170^{\circ}$ kis $1000$ K.[7] $110^{\circ}K$ [5] In a Carnot engine, when $T_{2} = 0^{\circ}C$ and $T_{2} = -200^{\circ}C$ , Its efficiency is $\eta_{1}$ and when $T_{1} = 0^{\circ}C$ and $T_{2} = -200^{\circ}C$ , Its efficiency is $\eta_{2}$ , then what is $\eta_{1}/\eta_{2}$ [1] $200 \text{ K}$ [2] $400 \text{ K}$ [3] $0.638$ [4] Cannot be calculated23.Even Carnot engine cannot give $100\%$ [6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[3] Reach absolute zero temperature		and rejects heat to	a sink at a temperature of					
[3] Q /2[4] 2Q /3127°C and sink temperature 27°C is 2[1] The temperature of sink of Carnot engine is 27°C. Efficiency of engine is 25%. Then temperature of source is [1] 227°C[2] 327°C[3] 127°C[2] 327°C[3] It is quite probable[1] 227°C[2] 327°C[3] It is quite probable[1] 227°C[2] 327°C[3] It is quite probable[3] 127°C[4] 27°C21.[4] 27°C[4] 27°C21.[5] 127°C[4] 27°C21.[6] The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K[2] 400 K[3] 500 K[2] 400 K[3] Transfer of heat by conduction [4] Isothermal compression[15.Ina Carnotengine, when $T_2 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ Efficiency of a Carnot engine is 50 temperature of intake the same temperature of outlet[1] 0.577[2] 0.733[3] 600 K[2] 400 K[3] 0.638[4] Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot[6.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[3] Reach absolute zero temperature		T/3. The amount o	f heat rejected is	20.	A scientist s	ays that t	he efficiency	of his heat
13.The temperature of sink of Carnot engine is $27^{\circ}$ C. Efficiency of engine is 25%. Then temperature of source is [1] 227°C [3] 127°C[1] It is impossible [2] It is possible but less probable [3] It is quite probable [4] Data is incomplete14.The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K [3] 500 K21.Which of the following processes is ref [1] Transfer of heat by radiation [2] Electrical heating of a nichrome w [3] Transfer of heat by conduction [4] Isothermal compression15.Ina Carnotengine, when $T_2 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [3] 0.638 [4] Cannot be calculated23.Efficiency of a Carnot engine cannot give 100% efficiency because we cannot [1] Prevent radiation [2] Find ideal [3] Reach absolute zero temperature		[1] Q /4	[2] Q /3		engine whic	h operate	es at source t	emperature
<ul> <li>13. The temperature of sink of Carnot engine is 27°C. Efficiency of engine is 25%. Then temperature of source is [1] 227°C [2] 327°C [3] 127°C [4] 27°C [4] 21 20°K [6] Electrical heating of a nichrome w [3] Transfer of heat by conduction [4] Isothermal compression [4] 200 K [1] 0.577 [2] 0.733 [3] 0.638 [4] Cannot be calculated [3] 600 K [4] 800 K [4] 80</li></ul>		[3] Q /2	[4] 2Q /3		127°C and s	ink tempe	rature 27°C is	s 26%, then
27°C. Efficiency of engine is 25%. Then temperature of source is[3] It is quite probable[1] 227°C[2] 327°C[3] 127°C[4] 27°C[3] 127°C[4] 27°C[3] 127°C[4] 27°C[4] Tansfer of heat by radiation[2] Electrical heating of a nichrome w operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K[2] 400 K[3] 500 K[4] 700 K[3] 500 K[4] 700 K[4] Isothermal compression[5] Ina Carnotengine, when $T_2 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ [4] Cannot be calculated23.[5] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures					[1] It is impo	ossible		
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[1] 227°C[2] 327°C[3] 127°C[4] 27°C21.Which of the following processes is re[1] Transfer of heat by radiation14.The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K[2] 400 K[3] 500 K[2] 400 K[3] 500 K[2] 400 K[3] 500 K[4] 700 K[4] roo K22.Efficiency of a Carnot engine is 50 temperature of outlet is 500 K. In increase efficiency up to 60%15.Ina Carnot engine, when $T_1 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [3] 0.638[4] Cannot be calculated23.16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures		27°C. Efficiency	of engine is 25%. Then		[3] It is quite	e probable	;	
[3] $127^{\circ}C$ [4] $27^{\circ}C$ 21.Which of the following processes is re [1] Transfer of heat by radiation14.The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K[2] 400 K[3] $500 \text{ K}$ [2] 400 K[3] Transfer of heat by conduction [4] Isothermal compression15.In a Carnot engine, when $T_2 = 0^{\circ}C$ and $T_1 = 200^{\circ}C$ , its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}C$ and $T_2 = -200^{\circ}C$ , Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [3] 0.638Efficiency of a Carnot engine is 50 temperature of outlet is 500 K. In increase efficiency up to 60% temperature of outlet16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures23.		temperature of sou	rce is		[4] Data is ir	ncomplete	;	
14.The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K [2] 400 K [3] 500 K[2] 400 K [3] 500 K[2] 400 K [4] 700 K[3] Transfer of heat by conduction [4] Isothermal compression15.Ina Carnot engine, when $T_2 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [1] 0.577 [2] 0.733Efficiency of a Carnot engine is 500 K. In increase efficiency up to 60% temperature of outlet is 500 K. In increase efficiency up to 60% temperature of outlet [1] 200 K [2] 400 K [3] 600 K16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures23.Even Carnot engine cannot give 100% efficiency because we cannot [3] Reach absolute zero temperature		[1] 227°C	[2] 327°C					
<ul> <li>14. The temperature of reservoir of Carnot's engine operating with an efficiency of 70% is 1000K. The temperature of its sink is <ul> <li>[1] 300 K</li> <li>[2] 400 K</li> <li>[3] 500 K</li> <li>[4] 700 K</li> </ul> </li> <li>15. Ina Carnot engine, when T<sub>2</sub>=0°C and T<sub>1</sub>=200°C, its efficiency is η<sub>1</sub> and when T<sub>1</sub> = 0°C and T<sub>2</sub>= - 200°C, Its efficiency is η<sub>2</sub>, then what is η<sub>1</sub>/η<sub>2</sub> <ul> <li>[1] 0.577</li> <li>[2] 0.733</li> <li>[3] 0.638</li> <li>[4] Cannot be calculated</li> </ul> </li> <li>16. The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures</li> </ul>		[3] 127°C	[4] 27°C	21.	Which of the	e followin	g processes is	s reversible
operating with an efficiency of 70% is 1000K. The temperature of its sink is [1] 300 K [2] 400 K [3] Transfer of heat by conduction [4] Isothermal compression [4] Isothermal compression [4] Isothermal compression [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [5] Transfer of heat by conduction [4] Isothermal compression [5] Transfer of heat by conduction [6] T						-		
The temperature of its sink is [1] 300 K [3] 500 K[2] 400 K [2] 400 K[4] Isothermal compression[1] 300 K [3] 500 K[2] 400 K [4] 700 K22.Efficiency of a Carnot engine is 50 temperature of outlet is 500 K. In increase efficiency up to 60% temperature of intake the same temperature of outlet15.Ina Carnot engine, when $T_2 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ [1] 0.577 [2] 0.733Even carnot engine content of outlet [1] 200 K [2] 400 K [3] 600 K[4] Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[1] Prevent radiation [2] Find ideal [3] Reach absolute zero temperature	14.	-	-			-		wire
[1] 300 K[2] 400 K[3] 500 K[4] 700 K[3] 500 K[4] 700 K[4] 700 K22.Efficiency of a Carnot engine is 50 temperature of outlet is 500 K. In increase efficiency up to 60% temperature of intake the same temperature of outlet15.In a Carnot engine, when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [1] 0.577[2] 0.733[3] 0.638[4] Cannot be calculated16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[3] Reach absolute zero temperature		* •	•			-		
[3] 500 K[4] 700 K22.Efficiency of a Carnot engine is 50 temperature of outlet is 500 K. In increase efficiency up to 60% temperature of intake the same temperature of outlet15.Ina Carnot engine, when $T_2 = 0^{\circ}$ C and $T_1 = 200^{\circ}$ C, its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [1] 0.577 [2] 0.733 [3] 0.638 [4] Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures23.Even Carnot engine cannot give 100% efficiency because we cannot		-	f its sink is		[4] Isotherm	al compre	ession	
15.In a Carnot engine, when $T_2 = 0^{\circ}C$ and $T_1 = 200^{\circ}C$ , its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}C$ and $T_2 = -200^{\circ}C$ , Its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ temperature of outlet is 500 K. In increase efficiency up to 60% temperature of outlet11. $T_2 = -200^{\circ}C$ , Its efficiency is $\eta_2$ , then what is $\eta_1/\eta_2$ Image: 11.12. $0.577$ [2] 0.733[3] 600 K[4] Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[3] Reach absolute zero temperature		[1] 300 K	[2] 400 K					
15.In a Carnot engine, when $T_2 = 0^{\circ}C$ and $T_1 = 200^{\circ}C$ , its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}C$ and $T_2 = -200^{\circ}C$ , Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ increase efficiency up to 60% temperature of intake the same temperature of outlet $11 0.577$ [2] 0.733[1] 200 K[2] 400 K[3] 0.638[4] Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[3] Reach absolute zero temperature		[3] 500 K	[4] 700 K	22.	-		-	
its efficiency is $\eta_1$ and when $T_1 = 0^{\circ}$ C and $T_2 = -200^{\circ}$ C, Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ [2] 0.733 [1] 200 K [2] 400 K [1] 0.577 [2] 0.733 [3] 0.638 [4] Cannot be calculated 23. Even Carnot engine cannot give 100% efficiency because we cannot 16. The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures [3] Reach absolute zero temperature					-			
$T_2 = -200^{\circ}C$ , Its efficiency is $\eta_2$ , then what is $\eta_1 / \eta_2$ temperature of outlet $[1] 0.577$ $[2] 0.733$ $[1] 200 K$ $[2] 400 K$ $[3] 0.638$ $[4]$ Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures $[1]$ Prevent radiation $[2]$ Find ideal[3] Reach absolute zero temperature	15.		2 1					
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$					-		ke the same	e what is
[1] 0.577[2] 0.733[3] 600 K[4] 800 K[3] 0.638[4] Cannot be calculated23.Even Carnot engine cannot give 100% efficiency because we cannot16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[1] Prevent radiation[2] Find ideal[3] Reach absolute zero temperature		$T_2 = -200^{\circ}C$ , Its	efficiency is $\eta_2$ , then what is		-	of outlet		
<ul> <li>[3] 0.638</li> <li>[4] Cannot be calculated</li> <li>23. Even Carnot engine cannot give 100% efficiency because we cannot</li> <li>16. The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures</li> <li>[3] Reach absolute zero temperature</li> </ul>					[1] 200 K		[2] 400 K	
<ul> <li>[4] Cannot be calculated</li> <li>[4] Cannot be calculated</li> <li>[4] Cannot be calculated</li> <li>[5] Even Carnot engine cannot give 100% efficiency because we cannot</li> <li>[6] The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures</li> <li>[7] Prevent radiation</li> <li>[8] Reach absolute zero temperature</li> </ul>			[2] 0.733		[3] 600 K		[4] 800 K	
16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperaturesefficiency because we cannot[1] Prevent radiation[2] Find ideal[3] Reach absolute zero temperature		[3] 0.638						
16.The efficiency of Carnot's engine operating between reservoirs, maintained at temperatures[1] Prevent radiation [3] Reach absolute zero temperature		[4] Cannot be calc	ulated	23.		-	-	0%
between reservoirs, maintained at temperatures [3] Reach absolute zero temperature					-			
	16.	-	• • •					
27°C and –123°C, is [4] Eliminate friction			-				o temperature	e
		27°C and –123°C,	is		[4] Eliminate	e friction		
One Academy 36, P. R.S Road, Chennimalai – 638051 PHONE: 096984 13524								87

	IE ACADEMY NEET SERIES	PHYSICS	- VOL II	Ι	CLASS-XII THERMODYNAMICS
24.	lower temperature	momentum mass	32.	and the compresse a temperature of 2 coefficient of perf [1] 5 [2] 8	
25.	-	es 3 x 10 <sup>6</sup> cal of heat from a and gives it to a sink at he by the engine is [2] 8.4 x 10 <sup>6</sup> J [4] Zero	22	The maximum po engine is [1] 1/2 [3] 3/4	perature 727°C and 227°C ossible efficiency of such an [2] 1/4 [4] 1.
26.	The first operation in [1] Isothermal expan [2] Adiabatic expans [3] Isothermal comp [4] Adiabatic compr	sion pression	33.	cyclebetween227	$[2] 6 \ge 10^4 \text{ cal}$
27.		on of working temperatures mot's engine is highest [2] 100K, 80K [4] 40 K, 20 K	34.	<ul><li>[1] Does not chan</li><li>[3] Decreases</li></ul>	crease or decrease depending
28.	temperature is $T_1$ a will be [1] $T_1 - T_2 / T_1$ [3] $T_1 - T_2 / T_2$	$[4] T_1/T_2$	35.	temperature T and reversibly at temp the following is co	ed reversibly to a system a l heat Q' is taken away from is perature T" then which one of orrect [2] $\frac{Q}{T} - \frac{Q'}{T} > 0$
29.	temperature $T_1$ and	ngine working between $T_2$ has an efficiency $\eta$ , the both the source and sink bled, will be [2] $\eta$ [4] $3\eta$ .		$[3] \frac{Q}{T} - \frac{Q'}{T} < 0$	ange in internal energy of th
30.	temperature of $-1$ performance of the e	tor has a freezer at a 3°C. The coefficient of ongine is 5. The temperature heat is rejected) will be [2] 325K [4] 320°C	36.	when the tempera that of sink is T Carnot's heat engin	<sup>2</sup> Carnot's heat engine is 0. ature of the source is $T_1$ and $T_2$ . The efficiency of anothe ne is also 0.5. The temperatur nk of the second engine ar

[3] 39°C [4] 320°C

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31. In a mechanical refrigerator, the low

 $[1] 2T_1, 2T_2$  $[3] T_1 + 5, T_2 - 5$   $\begin{array}{l} [2] \ 2T_1, \ T_2/2 \\ [4] \ T_1 + \ 10, \ T_2 - \ 10 \end{array}$ 

[] CLASS- XII THERMODYNAMICS
[1] S1 [2] S3 [3] S2 [4] S4
A Carnot engine operating between temperatures $T_1$ and $T_2$ has efficiency 1/6 When $T_2$ is lowered by 62 K, its efficiency increases to 1/3. Then $T_1$ and $T_2$ are, respectively [1] 372 K and 310 K [2] 372 K and 330 K [3] 330 K and 268 K [4] 310 K and 248 K
200 cal of heat is given to a heat engine so tha at rejects 150 cal of heat, if source temperature as 400 K, then the sink temperature is [1] 300 K [2] 200 K [3] 100 K [4] 50 K
A carnot engine, whose efficiency is 40% takes in heat from a source maintained at a temperature of 500K. It is desired to have an engine of efficiency 60%. Then, the intake temperature for the same exhaust (sink) temperature must be [1] Efficiency of carnot engine cannot be made larger than 50%
2] 1200 K 3] 750 K 4]600 K
<ul> <li>Which of the following is a true statement</li> <li>[1] The total entropy of thermally interacting systems is conserved</li> <li>[2] Carnot engine has 100% efficiency</li> <li>[3] Total entropy does not change in a reversible process</li> <li>[4] Total entropy in an irreversible process car either increase or decrease</li> </ul>

# Exercise – 1

# First Law of Thermodynamics ( $\Delta \mathbf{Q} = \Delta \mathbf{U} + \Delta \mathbf{W}$ )

Q	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15
Α	1	3	2	3	5	2	1	4	1	1	3	3	4	1	2
Q	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
Α	2	3	4	4	1	1	3	2	1	4	4	1	2	4	1
Q	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45
Α	2	1	1	1	1	2	3	3	2	1	3	1	1	3	3
Q	46	47	48	49	50										
Α	1	2	2	2	4										

# **ISOTHERMAL PROCESS**

Q	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15
Α	3	5	3	4	2	2	3	4	3	3	1	4	1	1	3
Q	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
A	3	1	3	1	3	2	2	1	1	1	3	2	2	2	1

# **ADIABATIC PROCESS**

Q	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15
Α	4	3	2	3	1	4	3	2	1	2	3	4	2	2	4
Q	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
Α	2	1	3	1	2	4	3	2	3	1	2	4	1	2	2
Q	31	32	33	34	35	36	37	38	39	40	41	42	43	44	45
Α	3	3	4	3	1	4	2	2	1	4	3	3	2	1	2
Q	46	47	48	49	50	51									
Α	4	2	4	2	1	4									

# **ISOBARIC AND ISOCHORIC PROCESSES**

Q	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15
A	1	3	2	2	2	2	3	2	4	3	3	3	2	1	4
Q	16	17	18	19	20	21									
Α	2	1	4	1	4	3									

# HEAT ENGINE, REFRIGERATOR AND SECOND LAW OF THERMODYNAMICS

Q	1	2	3	4	5	6	7	8	9	10	11	12	13	14	15
Α	4	3	2	4	1	1	2	2	4	2	3	2	3	1	1
Q	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
Α	1	3	4	2	1	4	2	3	1	2	1	4	1	2	3
	31	32	33	34	35	36	37	38	39	40	41	42	43		
Q	51	52	55	54	55	50	57	50	59	40	41	74	43		